academic**Journals**

Vol. 13(46), pp. 4320-4329, 12 November, 2014 DOI: 10.5897/AJB11.079 Article Number: CCF834A48569 ISSN 1684-5315 Copyright © 2014 Author(s) retain the copyright of this article http://www.academicjournals.org/AJB

Full Length Research Paper

Evaluation of some handling and processing parameters for briquetting of guinea corn (*Sorghum bi-color*) residue

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Received 1 July, 2011; Accepted 25 April, 2012

Biomass materials require reduction and densification for the purpose of handling and space requirements. Guinea corn (*Sorghum bi-color*) is a major source of biomass material in the tropic regions. The densification process involves some measurable parameters, namely: pressure, particles size and binder ratio. Guinea corn residue was collected from the Teaching and Research Farm of the Federal Polytechnic at Bida in Nigeria. The moisture content was 9.08% dry basis (db). It was reduced and sieved into three particle sizes D_1 (4.70 mm), D_2 (1.70 mm) and D_3 (0.60 mm). Starch paste of 40, 45, 50 and 55% was added as binder. Briquettes were produced using a hydraulic press and a cylindrical die (56 mm ϕ) at the processing pressures of 7.5, 8.5, 9.5 and 10.5 Megapascal (MPa). The bulk density of the unprocessed material was 46.03 kg/m³. The mean relaxed briquettes bulk density was 208.15 kg/m³, which reflects a volume reduction of about 450%. The maximum density of the briquettes ranged from 789 to 1372 kg/m³. For the expansion characteristics, the maximum and minimum axial relaxation occurred in the first 30 min of the extrusion. All the processing parameters were found to be significant at P<0.05 test level for all the measured characteristics. The briquettes were kept for six months under ambient condition without deterioration.

Key words: Guinea corn, briquettes, residue, parameters.

INTRODUCTION

Mechanics of agricultural material as a scientific discipline is presently being developed. For now, there are many process-material interactions that do not have exact methods of representation. Nevertheless, the experimental methods developed so far, can somehow be used successfully to select, design and optimize machines, (Sitkei. 1986). Heinimo (2008) postulated that at present, biomass covers approximately 11% of the global total primary energy consumption of slightly more than 430 EJ/year. Briquetting of forest products, agricultural wastes and rural-agro industrial residues has long been recognized as a viable technology for

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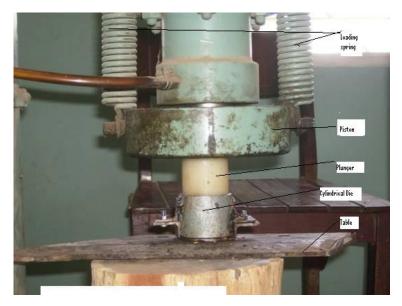


Figure 1. Hydraulic powered press fitted with plunger and cylinder die.

alternative energy generation (Resch, 1982). This statement is also buttressed by Gurkan et al. (2010). Briquetting technology is fast gaining prominence in the world of science today because of its numerous advantages of helping to densify very bulky (low density) materials, particularly those of biomass origin.

The compaction of agricultural residues into briguettes in general terms improves the economics of material handling, transportation and storage, thereby enhancing more versatile application in use. Munoz-Hernandez et al. (2004), identified some methods of achieving densification using commercial machines which include bailing, cubing, pelleting and briquetting; by means of piston, extrusion screws or by roll presses. Furthermore, it was identified that one of the requirements to design, construct and improve densification system is based mainly on the knowledge of suitable levels of process variables such as die geometry, relaxation time, die and material temperature and pressure. Other material variables include moisture content and its distribution, size and shape of the particles, size distribution of the particles, biochemical and mechanical characteristic (Rehkugler and Buchele, 1969). Although the effect of binder is still under intense research, Tabil et al. (1997) concluded that, there exists little scientific information related to the effectiveness of binders. However, a few researchers have postulated that at relatively low pressure application, the effect of binder might enhance densification. Starch has been used as a binding agent for briquetting of Rattan furniture waste and guinea corn bi-color) (Olorunshola, (Sorghum residue 2004; Bamgboye and Bolufawi, 2009).

Some researchers have used mechanical elements of commercial machines as experimental prototypes for densification, but the constraints here include, cost of instrumentation and large volumes of materials required for the experiment. Experimental tests by means of presses and laboratory dies for densification have offered easier and less expensive ways to conduct experimental tests under controlled conditions. Under laboratory conditions, technical information needed for economic and technical decisions can be obtained; for instance, in a closed-end die, the temperature and the use of binder can be controlled with high precision such as achieved by Faborode and O'Callaghan (1987) and Mohsenin and Zaske (1976).

The main objectives of this work was to find the levels of some selected processing parameters that provide optimum responses in terms of some measured post briquetting characteristics in briquetting of guinea corn residue. The parameters selected include pressure, particle size distribution, binder quantity and dwell-time.

MATERIALS AND METHODS

A 3 x 4 x 4 randomized complete block design (RCBD) experiment was used to synchronize the parameters of pressure (P), particle size (D) and binder/residue ratio (B) (Gomez and Gomez, 1983) adopting a dwell-time of 90 s. The operating pressures were 7.5, 8.5, 9.5 and 10.5 Megapascal (MPa). The particle size distribution was obtained by size reduction (milling) and sieve analysis. The particle sizes obtained were distributed into three categories: D₁ = 4.70 mm, D₂ = 1.70 mm and D₃ = 0.60mm. The binder/residue ratio was 40, 45, 50 and 55% by weight of binder/residue. Each sample briquette was produced using a fixed die charge packed in a steel cylinder 56 mm diameter positioned and compressed in a hydraulic press as shown in Figure 1. The briquettes formed are displayed in Figure 2.

Some measured characteristics of the briquettes included the bulk and initial densities, maximum and relaxed densities and the rate of expansion. The compaction energies were also determined.

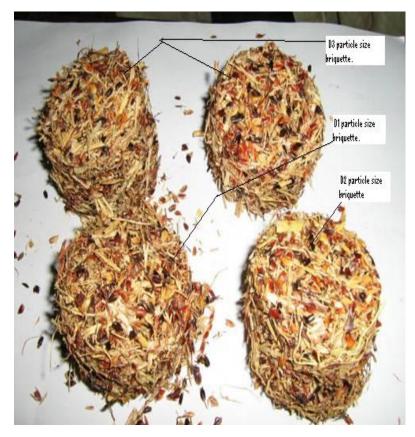


Figure 2. Briquettes produced form the hydraulic press.

Table 1.	Initial	density	(Y_{o})	Kg/m ³ .
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Binder ratio (%)	Particle size D ₁ (4.7 mm)	Particle size D ₂ (1.7 mm)	Particle size D₃ (0.6 mm)
B ₁	141	208	175
B ₂	149	212	205
B ₃	146	216	246
B ₄	140	247	250

P, Pressure in Megapascal (MPa); D, particle size in mm; B, binder ratio; Y, density kg/m³; r, Y_d/Y_o ; r_d , Y_r/Y_d ; r_r , $1/r_d$.

Other characteristics determined included compaction ratio (r) and relaxation ratio (r_r) which are derivatives of the initial, maximum and relaxed densities. The readings were treated statistically using, means and analysis of variance (ANOVA). Correlation and regression analysis were used to streamline the statistically treated data. The various densities and expansion rates were subjected to ANOVA test to determine the level of significance of the processing parameters (P, D and B) for the measured characteristics. The shelf live was estimated after observing the briquette for the period of six months under ambient condition.

RESULTS AND DISCUSSION

The various densities are in kg/m^3 : initial density (Y_o) (zero pressure application), maximum density (Y_d) (in-die

density) and relaxed density (Y_r) are displayed in Tables 1, 2 (a, b and c) and 3 (a, b and c).

A careful study of the data in Tables 1 to 3 reveal the following observations: the maximum densities for the particle size D_1 , D_2 and D_3 varied from 798 to 1372 kg/m³ as shown in Tables 2a, b and c. These values are much higher than the initial densities of the uncompressed mixture (141 to 250 kg/m³) shown in Table 1. Thus, this process has been able to obtain improved density which is a desirable factor in briquetting. The bulk density of the unprocessed material was 46.03 kg/m³ while the mean bulk density of the relaxed briquette was 208.15 kg/m³, reflecting a volume reduction of about 450%. An increase in the maximum density was observed for all the particle

Table 2a.	Maximum	density	(Y_d)	Kg/m ³	(D ₁).
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Binder ratio (%)	P 1	P ₂	P ₃	P ₄
B ₁	1161	1204	1292	1372
B ₂	1018	1074	1192	1307
B ₃	899	924	987	1050
B ₄	789	888	917	1015

P, Pressure in Megapascal (MPa); D, particle size in mm; B, binder ratio; Y, density kg/m³; r, Y_d/Y_o; r_d , Y_r/Y_d; r_r , 1/ r_d .

Table 2b. Maximum density (Y_d) Kg/m³ (D₂).

Binder ratio (%)	P ₁	P ₂	P ₃	P ₄
B ₁	917	980	1030	1110
B ₂	899	960	996	1093
B ₃	892	932	994	1053
B ₄	872	911	932	938

P, Pressure in Megapascal (MPa); D, particle size in mm; B, binder ratio; Y, density kg/m³; r, Y_d/Y_o; r_d, Y_r/Y_d; r_r, 1/r_d.

Table 2c. Maximum density (Y_d) Kg/m³ (D_3) .

Binder ratio (%)	P ₁	P ₂	P ₃	P ₄
B ₁	821	960	1015	1093
B ₂	789	928	960	980
B ₃	789	861	917	960

P, Pressure in Megapascal (MPa); D, particle size in mm; B, binder ratio; Y, density kg/m³; r, Y_d/Y₀; r_d, Y_r/Y_d; r_r, 1/r_d.

Binder ratio (%)	P 1	P ₂	P ₃	P ₄
B1	235	242	244	248
B ₂	238	240	244	235
B ₃	239	240	240	238
B ₄	281	304	289	292

Table 3a. Relaxed density (Y_r) Kg/m³ (D₁).

P, Pressure in Megapascal (MPa); D, particle size in mm; B, binder ratio; Y, density kg/m³; r, Y_d/Y_o; r_d, Y_r/Y_d; r_r, 1/r_d.

Binder ratio (%)	P ₁	P ₂	P ₃	P ₄
B ₁	347	357	352	248
B ₂	334	334	328	245
B ₃	329	330	325	243
B ₄	324	323	323	292

Table 3b. Relaxed density (Y_r) Kg/m³ (D₂).

P, Pressure in Megapascal (MPa); D, particle size in mm; B, binder ratio; Y, density kg/m³; r, Y_d/Y_o ; r_d , Y_r/Y_d ; r_r , $1/r_d$.

Binder ratio (%)	P ₁	P ₂	P ₃	P ₄
B ₁	389	405	415	436
B ₂	427	435	424	433
B ₃	388	400	397	406

Table 3c. Relaxed density Kg/m³ (D₃).

P, Pressure in Megapascal (MPa); D, particle size in mm; B, binder ratio; Y, density kg/m³; r, Y_d/Y_o; r_d, Y_r/Y_d; r_r, 1/r_d.

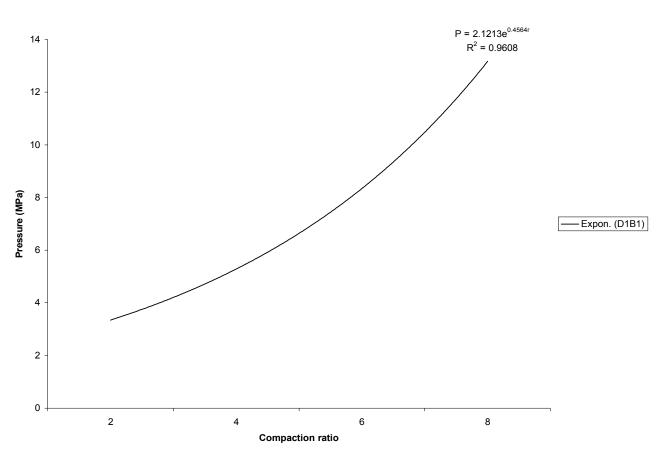


Figure 3. Relationship between pressure and compression ratio for D₁B₁.

sizes with increasing pressure. A decrease in density was also observed with increasing binder ratio. The relaxed briquette densities shown in Tables 3a, b and c were smaller than the recorded maximum densities because of the expansion of the briquette after extrusion.

The ANOVA showed that the effect of the processing parameters, pressure, binder ratio and particle size were significant at P < 0.05. The relationship between the selected parameters and some measured characteristics are as shown in Figures 3 to 10. The effects of pressure and compaction ratio on the particle sizes of the material are graphically shown in Figures 3 to 5. The graphs are exponential in nature. The area under each curve in Figures 3 to 5 are estimates of the compaction energy. The energies of compaction are found to reduce with reducing particle size dimension. The rates of expansion

of the briquettes considering the binder ratio at the background are illustrated by Figures 6 and 7. It was observed that the most rapid rate of expansion took place in the first 100 min after extrusion. Figures 8 to 10 showed the effect of binder on maximum and relaxed density for briquettes with D_1 D_2 and D_3 particle size. For the expansion characteristic (axial relaxation), the maximum and minimum axial relaxation occurred in the first 30 min of the extrusion with values 138.64 and 28.0% in the longitudinal axis while the maximum and minimum radial relaxation were 11.50 and 4.0%, respectively. For briquettes with D_1 particle size, the maximum density decreases with increasing binder ratio indicating that more of the spaces have been filled with binder materials which to some extent is not compressible. The relaxed density does not exhibit the phenomenon

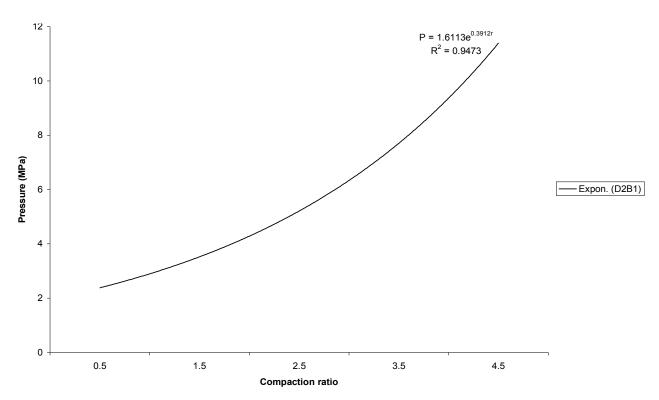


Figure 4. Relationship between pressure and compression ratio for D₂B₁.

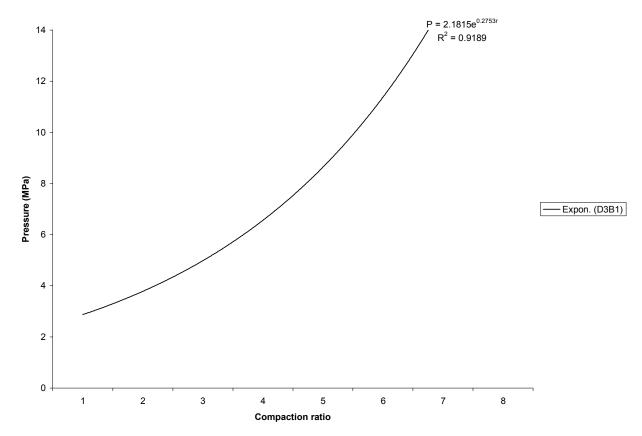


Figure 5. Relationship between pressure and compression ratio for D₃B₁.

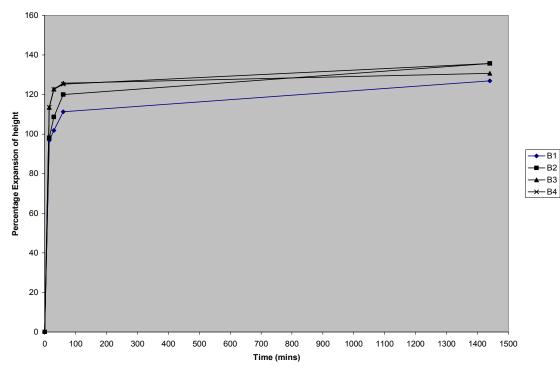


Figure 6. Percentage rate of expansion of briquettes with binder ratio (D₂P₁).

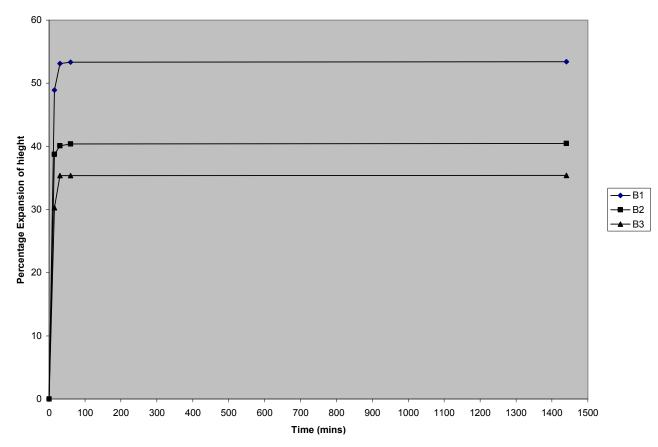


Figure 7. Percentage rate of expansion of briquettes with binder ratio (D₃P₁).

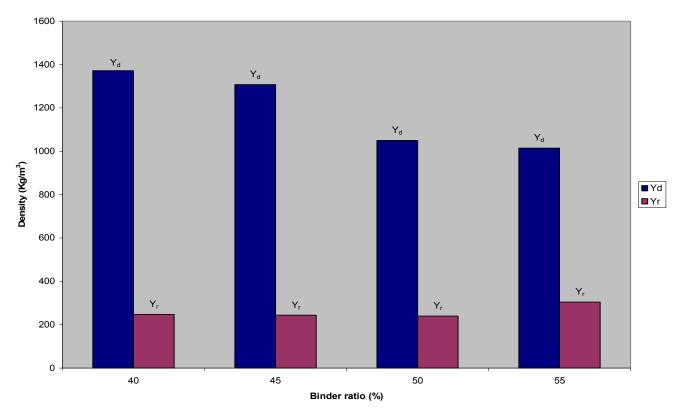


Figure 8. Effect of binder ratio on maximum and relaxed density for D₁ particle size briquettes.

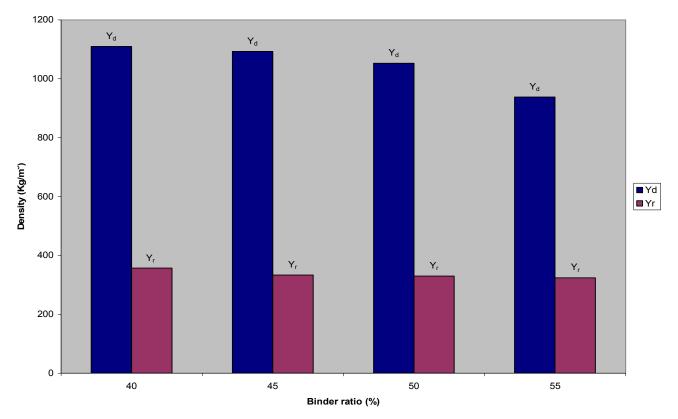


Figure 9. Effect of binder ratio on maximum and relaxed density for D_2 particle size briquettes.

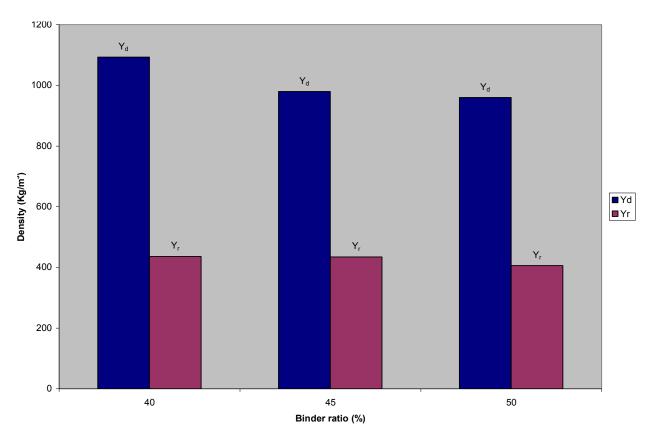


Figure 10. Effect of binder ratio on maximum and relaxed density for D₃ particle size briquettes.

raised above. For D_2 particle size briquettes, there is very little variation in the maximum and relaxed densities.

This phenomenon is traceable to the lustre surface nature of the particle size. For the briquettes with D_3 particle size, the trend was similar to what was observed for D_2 particle size briquettes even though the particles were finer. The briquettes that were kept for shelf life examination did not disintegrate appreciably over a period of about six months, when visually inspected and physically handled.

Conclusion

The measured characteristics indicated that each and every one of the processing parameters of pressure, particle size and binder ratio have singularly or corporately affected the values of the measured characteristics. The compaction energy was directly related to the particle size more than the other processing parameters of pressure and binder ratio. Less compaction energy was recorded for smaller particle size compression process. A large volume reduction (450%) of the material was achievable by these processes. All the processing parameters were found to be significant at p < 0.05 for all the measured characteristics. If the right combination of the handling and processing parameters are applied to the materials, the briquettes can be sustained for a long period. For further work, energy balance for size reduction and compression process could be determined by investigation.

Conflict of Interests

The author(s) have not declared any conflict of interests.

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