International Journal of Engineering, Science and Technology Vol. 12, No. 1, 2020, pp. 38-53



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Finite element numerical investigation into unsteady MHD radiating and reacting mixed convection past an impulsively started oscillating plate

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Abstract

In this article, numerical investigation is carried out for the unsteady MHD mixed convection flow of radiating and chemically reacting fluid past an impulsively started oscillating vertical plate with variable temperature and constant mass diffusion. The transport model employed includes the Hall current. A uniform magnetic field is applied transversely to the direction of the fluid flow. The flow consideration is subject to small magnetic Reynolds number. The Rosseland approximation is used to describe the radiation heat flux in the energy equation. The dimensionless governing system of partial differential equations of the flow has been solved numerically by employing the finite element method. The influence of pertinent parameters on primary velocity, secondary velocity, temperature and concentration are presented graphically whereas primary skin friction, secondary skin friction, Nusselt number and Sherwood number are presented in tabular form. A comparison of the present method was made with the exact solution obtained by Rajput and Kanaujia (2016) by considering primary and secondary skin frictions, it was noticed that a very good agreement.

Keywords: MHD, radiation parameter, chemical reaction parameter, magnetic parameter, Hall current.

DOI: http://dx.doi.org/10.4314/ijest.v12i1.4

1. Introduction

The study of MHD with heat and mass diffusion in the presence of radiation has attracted the attention of a large number of researchers due to its diverse applications. Many processes in new engineering occur at high temperature and knowledge of radiation heat transfer becomes necessary for the design of the pertinent equipment. Nuclear power plants, gas turbines and the various propulsion devices for aircraft, missiles, satellites, and space vehicles, etc are examples of such engineering areas. Muthucumaraswamy and Janakiraman (2006) studied MHD and radiation effects on moving isothermal vertical plate with variable mass diffusion. Rajesh and Varma (2010) presented radiation effects on MHD flow through a porous medium with variable temperature and mass diffusion. Mebine and Adigio (2011) analyzed thermal radiation effects on transient MHD free convection flow over a vertical surface embedded in a porous medium with variable temperature and mass diffusion. Nandkeolyar et. al (2013) studied unsteady hydro-magnetic natural convection flow of a dusty fluid past an impulsively moving vertical plate with ramped temperature in the presence of thermal radiation. Thermo-dynamic analysis of unsteady MHD mixed convection with slip and thermal radiation over a permeable surface were reported by Muhammad and Makinde (2017).

In all the above cited studies, the effects of chemical reaction on the flow are not taken into account. Investigation of MHD flow with chemical reaction is of much significance due to its wide applications in many branches of science and engineering. In many chemical engineering processes, chemical reaction takes place between a foreign mass and the working fluid in which the plate is moving. These processes take place in numerous industrial applications such as manufacturing of ceramics or glassware, polymer production and food processing. In nature, the presence of pure air or water is not possible. Some foreign mass may be present

either naturally or mixed with the air or water. The presence of a foreign mass in air or water causes some kind of chemical reaction. Theoretical study of chemical reaction effects on vertical oscillating plate with variable temperature were presented by Muthucumaraswamy and Meenakshisundaram (2006). Muthucumaraswamy and Janakiraman (2008) examined the mass transfer effects on isothermal vertical oscillating plate in the presence of chemical reaction. Mahapatra et. al (2010) analyzed the effects of chemical reaction on free convection flow through a porous medium bounded by a vertical surface. Rajesh and Varma (2010) investigated the chemical reaction effects on free convection flow past an exponentially accelerated vertical plate. Effects of chemical reaction on the unsteady free convection flow past an infinite vertical permeable moving plate with variable temperature was analyzed by El-Fayez (2012). Sehkar and Reddy (2012) presented the effects of chemical reaction on MHD free convective oscillatory flow past a porous plate with viscous dissipation and heat sink. Makinde (2012) studied chemically reacting hydromagnetic unsteady flow of radiating fluid past a vertical plate with constant heat flux. Jayakar et. al (2018) investigated thermo-diffusion effects on MHD chemically reacting fluid flow past an inclined porous plate in a slip flow regime.

However, in all these investigations, the effects of Hall current are not taken into account. The effect of Hall current cannot be completely ignored if the strength of the magnetic field is strong and number of density electrons is small as it is responsible for the charge of the flow pattern of an ionized gas. Hall current results in a development of an additional potential difference between opposite surfaces of a conductor for which a current is induced perpendicular to both the electric and magnetic field. This current is known as Hall current. It plays an important role in determining features of the fluid flow problems because it induces secondary flow in the flow field. Sharma et. al (2007) analyzed the effects of Hall current on MHD mixed convection flow of a viscous incompressible fluid past a vertical porous plate immersed in a porous medium with heat source/sink. Maguna and Mutua (2013) presented the Hall current effects on free convection flow and mass transfer past a semi infinite vertical flat plate. Hall and rotation effects on MHD flow past an exponentially accelerated vertical plate with variable temperature and mass diffusion in the presence of Hall current was studied by Rajput and Kanaujia (2016). Recently, Reddy (2018) presented Hall effect on MHD transient flow past an impulsively started infinite horizontal porous plate in a rotating system.

The objective of the present work is to study the unsteady MHD mixed convection flow past an impulsively started oscillating vertical plate with radiation, chemical reaction and Hall current. The finite element method has been adopted to solve the governing equations of the flow. The effects of embedded parameters on primary and secondary fluid velocities, fluid temperature, fluid concentration, primary and secondary skin frictions, Nusselt number and Sherwood number are presented through the graphs and tables and then discussed. According to the best of authors' knowledge this work not yet received the attention of researchers though it has significant applications in the fields of science and engineering.

2. Model Problem

Consider the unsteady MHD flow of viscous incompressible electrically conducting, radiating and reacting fluid past an

impulsively started oscillating infinite vertical plate. A uniform magnetic field \overrightarrow{B} of strength B_0 is applied in the direction perpendicular to the fluid flow. In the Cartesian co-ordinate system, the x'-axis is taken along the plate in the vertically upward direction, the y'-axis perpendicular to the direction of the plate and the z'-axis is normal to the x'y'-plane. The physical model of the problem is shown in Fig.1. Initially, at time $t' \le 0$, the temperature of the fluid and the plate is T_{∞}' and the concentration of the fluid is C_{∞}' . Subsequently, at time t' > 0, the plate starts oscillating in its own plane with frequency \breve{S}' , the temperature of the plate and the concentration of the fluid, respectively are raised to T_w' and C_w' . It is assumed that the radiation heat flux in the x'direction is negligible as compared to that in y'- direction. As the plate is of infinite extent and electrically non-conducting, all the physical quantities, except the pressure, are functions of y' and t'.

The generalized Ohm's law on taking Hall current into account Cowling (1957) is given by

$$\vec{J} + \frac{S_e t_e}{B_0} (\vec{J} \times \vec{B}) = \dagger (\vec{B} + \vec{q} \times \vec{B})$$
(1)

where $\vec{q}, \vec{B}, \vec{E}, \vec{J}, \dagger, \vec{S}_e$ and \ddagger_e are respectively, velocity vector, magnetic field vector, electric field vector, current density vector, electric conductively, cyclotron frequency and electron collision time. The equation of continuity $\nabla \cdot \vec{q} = 0$ gives v' = 0 everywhere in the flow since there is no variation of the flow in y'-direction, where $\vec{q} = (u', v', w')$ and u', v', w' are respectively, velocity components along the coordinate axes.

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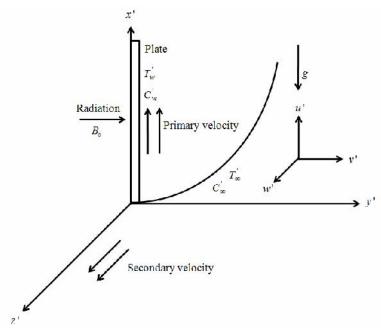


Figure 1. Physical model and coordinate system.

The magnetic Reynolds number is so small that the induced magnetic field produced by the fluid motion is neglected. The solenoid relation $\nabla \cdot \vec{B} = 0$ for the magnetic field $\vec{B} = (B_{x'}, B_{y'}, B_{z'})$ gives $B_{y'} = \text{constant say } B_0$. i.e., $\vec{B} = (0, B_0, 0)$ everywhere in the flow. The conservation of electric current $\nabla \cdot \vec{J} = 0$ yields $j_{y'} = \text{constant}$, where $\vec{J} = (j_{x'}, j_{y'}, j_{z'})$. This constant is zero since $j_{y'} = 0$ at the plate which is electrically non-conducting. Hence, $j_{y'} = 0$ everywhere in the flow. In view of the above assumption, Eq. (1) yields

$$j_{x'} - m j_{y'} = \dagger (E_{x'} - w' B_0)$$
⁽²⁾

$$j_{z'} + mj_{x'} = \dagger (E_{z'} + u'B_0) \tag{3}$$

where $m(=\check{S}_e \dagger_e)$ is the Hall parameter which represents the ratio of electron-cyclotron frequency and the electron-atom collision

frequency. Since the induced magnetic field is neglected, Maxwell equation $\nabla \times \vec{E} = -\frac{\partial \vec{H}}{\partial t}$ becomes $\nabla \times \vec{E} = 0$ which gives

 $\frac{\partial E_{x'}}{\partial y'} = 0$ and $\frac{\partial E_{z'}}{\partial y'} = 0$. This implies that $E_{x'} = \text{constant}$ and $E_{z'} = \text{constant}$ everywhere in the flow and choose this constants equals to zero, i.e., $E_{x'} = E_{z'} = 0$. Solving for $j_{x'}$ and $j_{z'}$ from Eqs. (2) and (3), on using $E_{x'} = E_{z'} = 0$,

$$j_{x'} = \frac{\dagger B_0}{1 + m^2} (mu' - w')$$
(4)

$$j_{z'} = \frac{1 D_0}{1 + m^2} (mw' + u')$$
(5)

Taking into consideration the assumptions made above, under the Boussinesq's approximation, and using Eqs. (4) and (5), the basic governing equations of the flow are derived as:

$$\frac{\partial u'}{\partial t'} = v \frac{\partial^2 u'}{\partial {y'}^2} - \frac{\dagger B_0^2}{\dots (1+m^2)} (u'+mw') + g S (T'-T_{\infty}) + g S^* (C'-C_{\infty})$$
(6)

$$\frac{\partial w'}{\partial t'} = v \frac{\partial^2 w'}{\partial y'^2} + \frac{\dagger B_0^2}{\dots (1+m^2)} (mu' - w')$$
(7)

$$\dots C_p \frac{\partial T'}{\partial t'} = k \frac{\partial^2 T'}{\partial y'^2} - \frac{\partial q_r}{\partial y'}$$
(8)

$$\frac{\partial C'}{\partial t'} = D \frac{\partial^2 C'}{\partial {v'}^2} - X'(C' - C'_{\infty})$$
(9)

The initial and boundary conditions for the problem are:

$$t' \le 0; u' = 0, w' = 0, T' = T_{\infty}', C' = C_{\infty}' \quad \text{for all } y' \ge 0$$

$$t' > 0; u' = u_0 \cos \tilde{S}'t', w' = 0, T' = T_{\infty}' + (T_w' - T_{\infty}') \frac{t' u_0^2}{\xi}, C' = C_w' \quad \text{at } y' = 0$$

$$u' \to 0, w' \to 0, T' \to T_{\infty}', C' \to C_{\infty}' \quad \text{as } y' \to \infty$$
(10)

The radiation heat flux q_r under the Rosseland approximation Magyari and Pantokratoras (2011) expressed by

$$q_r = -\frac{4t^*}{3k^*} \frac{\partial T'^4}{\partial y'}$$
(11)

where \uparrow^* is the Stefan-Boltzmann constant and k^* is the mean absorption coefficient. It is assumed that temperature difference within the flow are sufficiently small, then Eq. (11) can be linearized by expanding T'^4 into the Taylor series about T'_{∞} which, after neglecting higher-order terms, takes the form:

$$T'^{4} \cong 4T_{\infty}'^{3}T' - 3T_{\infty}'^{4} \tag{12}$$

In view of Eqs. (11) and (12), Eq. (8) reduces to

$$\dots C_{p} \frac{\partial T'}{\partial t'} = k \left(1 + \frac{16\dagger^{*} T^{3}_{\infty}}{3kk^{*}} \right) \frac{\partial^{2} T'}{\partial y^{2}}$$
(13)

Let us introduce the following non-dimensional parameters and quantities:

$$u = \frac{u'}{u_0}, y = \frac{y'u_0}{v}, t = \frac{t'u_0^2}{v}, w = \frac{w'}{u_0}, \tilde{S} = \frac{\tilde{S}'v}{u_0^2}, S_c = \frac{v}{D}, P_r = \frac{-C_p}{k}, M = \frac{t}{u_0^2}, X = \frac{X'v}{u_0^2}, X = \frac{X'v}{u_0^2}, R = \frac{16t^*T_{\infty}^{'3}}{3kk^*}, w = \frac{(T' - T_{\infty})}{(T_w' - T_{\infty})}, W = \frac{(C' - C_{\infty})}{(C_w' - C_{\infty})}, G_r = \frac{gS\in(T_w' - T_{\infty})}{u_0^3}, G_m = \frac{gS\in(C_w' - C_{\infty})}{u_0^3}$$
(14)

Using Eq. (14), into Eqs. (6), (7), (9) and (13), the following dimensionless governing equations of the flow are obtained:

$$\frac{\partial u}{\partial t} = \frac{\partial^2 u}{\partial y^2} - \frac{M}{(1+m^2)}(u+mw) + G_{r''} + G_m W$$
(15)

$$\frac{\partial w}{\partial t} = \frac{\partial^2 w}{\partial y^2} + \frac{M}{(1+m^2)}(mu-w)$$
(16)

$$\frac{\partial_n}{\partial x} = \frac{(1+R)}{R} \frac{\partial_n^2}{\partial x^2}$$
(17)

$$\frac{\partial W}{\partial t} = \frac{1}{S_c} \frac{\partial^2 W}{\partial y^2} - XW$$
(18)

The initial and boundary conditions Eq. (10), in non-dimensional form become:

$$t \le 0; u = 0, w = 0, _{\#} = 0, W = 0 \qquad \text{for all } y \ge 0$$

$$t > 0; u = \cos \check{S}t, w = 0, _{\#} = t, W = 1 \qquad \text{at } y = 0$$

$$u \to 0, w \to 0, _{\#} \to 0, W \to 0 \qquad \text{as } y \to \infty$$
(19)

3. Numerical Procedure

The dimensionless governing system of partial differential equations given in Eqs. (15) - (18), subject to initial and boundary conditions Eq, (19) are solved numerically for various values of parameters involved in the problem by using the finite element method. The finite element method is extremely efficient technique to solve ordinary and partial differential equations which occurs in wide range of engineering problems such as fluid mechanics, heat transfer, electrical systems, solid mechanics and chemical engineering, etc. Detailed discussion of the method is given in Zienkiewiez (1971), Reddy (1985) and Bathe (1996).

Variational Formulation

The variational form associated with Eqs. (15) – (18), over a typical two nodded linear element $(e), (y_j \le y \le y_k)$ is given by

$$\int_{y_{j}}^{y_{k}} w_{1} \left[\left(\frac{\partial u}{\partial t} \right) - \left(\frac{\partial^{2} u}{\partial y^{2}} \right) + \frac{M}{\left(1 + m^{2} \right)} \left(u + mw \right) - \left(G_{r^{u}} + G_{m}W \right) \right] dy = 0$$
(20)

$$\int_{y_j}^{y_k} w_2 \left[\left(\frac{\partial w}{\partial t} \right) - \left(\frac{\partial^2 w}{\partial y^2} \right) + \frac{M}{\left(1 + m^2 \right)} \left(mu - w \right) \right] dy = 0$$
(21)

$$\int_{y_j}^{y_k} w_3 \left[\left(\frac{\partial_{n}}{\partial t} \right) - \frac{(1+R)}{P_r} \left(\frac{\partial^2_{n}}{\partial y^2} \right) \right] dy = 0$$
(22)

$$\int_{y_i}^{y_k} w_4 \left[\left(\frac{\partial W}{\partial t} \right) - \frac{1}{S_c} \left(\frac{\partial^2 W}{\partial y^2} \right) + XW \right] dy = 0$$
(23)

where w_1, w_2, w_3 and w_4 are arbitrary test functions and may be viewed as the variations in u, w, w, w and w, respectively. After reducing the order of integration and non-linearity, the following equations are obtained:

$$\int_{y_{j}}^{y_{k}} \left[\left(\frac{\partial w_{1}}{\partial y} \right) \left(\frac{\partial u}{\partial y} \right) + w_{1} \left(\frac{\partial u}{\partial t} \right) + \frac{M}{\left(1 + m^{2} \right)} w_{1} \left(u + mw \right) \right] dy - \left[w_{1} \left(\frac{\partial u}{\partial y} \right) \right]_{y_{j}}^{y_{k}} = 0$$

$$(24)$$

$$\int_{y_j}^{y_k} \left[\left(\frac{\partial w_2}{\partial y} \right) \left(\frac{\partial w}{\partial y} \right) + w_2 \left(\frac{\partial w}{\partial t} \right) + \frac{M}{\left(1 + m^2 \right)} w_2 \left(mu - w \right) \right] dy - \left[w_2 \left(\frac{\partial w}{\partial y} \right) \right]_{y_j}^{y_k} = 0$$
(25)

$$\int_{y_j}^{y_k} \left[\frac{(1+R)}{P_r} \left(\frac{\partial w_3}{\partial y} \right) \left(\frac{\partial_{y}}{\partial y} \right) + w_3 \left(\frac{\partial_{y}}{\partial t} \right) \right] dy - \frac{(1+R)}{P_r} \left[w_3 \left(\frac{\partial_{y}}{\partial y} \right) \right]_{y_j}^{y_k} = 0$$
(26)

$$\int_{y_j}^{y_k} \left[\frac{1}{S_c} \left(\frac{\partial w_4}{\partial y} \right) \left(\frac{\partial w}{\partial y} \right) + w_4 \left(\frac{\partial w}{\partial t} \right) - (\mathbf{X} \mathbf{W}) w_4 \right] dy - \frac{1}{S_c} \left[w_4 \left(\frac{\partial w}{\partial y} \right) \right]_{y_j}^{y_k} = 0$$
(27)

Finite Element Formulation

The finite element model may be obtained from Eqs. (24) – (27) by substituting appropriate finite element approximations over the element $(e), (y_j \le y \le y_k)$ of the form:

$$u^{(e)} = \sum_{j=1}^{2} u_j \mathbb{E}_j, w^{(e)} = \sum_{j=1}^{2} w_j \mathbb{E}_k, w^{(e)} = \sum_{j=1}^{2} w_j \mathbb{E}_j, w^{(e)} = \sum_{j=1}^{2} w_j \mathbb{E}_j$$
(28)

with $w_1 = w_2 = w_3 = w_4 = \mathbb{E}_j (j = 1, 2)$ where u_j, w_j, w_j and w_j are, respectively, primary fluid velocity, secondary fluid velocity, fluid temperature and fluid concentration at j^{th} node of the element (e) and \mathbb{E}_j 's are the shape functions for a typical element (e), $(y_j \le y \le y_k)$ and are taken as:

$$\mathbb{E}_{j} = \frac{y_{k} - y}{y_{k} - y_{j}} \quad \text{and} \quad \mathbb{E}_{k} = \frac{y - y_{j}}{y_{k} - y_{j}}, \quad \left(y_{j} \le y \le y_{k}\right)$$
(29)

Using Eqs. (28) and (29) into Eqs. (24) to (27), after assembly of all the element equations by inter-element connectivity conditions and using Eq. (19), we obtain the following tri-diagonal system of equations: $Au = A'; Bw = B'; C_u = C'; Dw = D'$ (30) where u, w, w and A', B', C', D' are column matrices having n - components, $u_i^{j+1}, w_i^{j+1}, w_i^{j+1}, w_i^{j+1}$ and $u_i^j, w_i^j, w_i^j, w_i^j$ respectively, and A, B, C and D are diagonal matrices of order -n whose elements are given by

$$a_{i-1,i} = 1 - 3r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; \\ b_{i-1,i} = 1 - 3r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; \\ c_{i-1,i} = \left(\frac{P_r}{1+R}\right) - 3r; \\ d_{i-1,i} = S_c - 3r + \frac{1}{2}rS_c x h^2 \quad \text{at } i = 2(1)n = 3r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; \\ c_{i,i} = 4 + 6r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; \\ b_{i,i} = 4 + 6r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; \\ c_{i,i} = 4\left(\frac{P_r}{1+R}\right) + 6r; \\ d_{i,i} = 4S_c + 6r + 2rS_c x h^2 \quad \text{at } i = 1(1)n = 3r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; \\ c_{i,i} = 4\left(\frac{P_r}{1+R}\right) + 6r; \\ d_{i,i} = 4S_c + 6r + 2rS_c x h^2 \quad \text{at } i = 1(1)n = 3r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; \\ c_{i,i} = 4\left(\frac{P_r}{1+R}\right) + 6r; \\ d_{i,i} = 4S_c + 6r + 2rS_c x h^2 \quad \text{at } i = 1(1)n = 3r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; \\ c_{i,i} = 4\left(\frac{P_r}{1+R}\right) + 6r; \\ d_{i,i} = 4S_c + 6r + 2rS_c x h^2 \quad \text{at } i = 1(1)n = 3r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; \\ c_{i,i} = 4\left(\frac{P_r}{1+R}\right) + 6r; \\ d_{i,i} = 4S_c + 6r + 2rS_c x h^2 \quad \text{at } i = 1(1)n = 3r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; \\ c_{i,i} = 4\left(\frac{P_r}{1+R}\right) + 6r; \\ d_{i,i} = 4S_c + 6r + 2rS_c x h^2 \quad \text{at } i = 1(1)n = 3r + \frac{1}{2}r\left(\frac{M}{1+R}\right)h^2; \\ c_{i,i} = 4\left(\frac{P_r}{1+R}\right) + 6r; \\ d_{i,i} = 4S_c + 6r + 2rS_c x h^2 \quad \text{at } i = 1(1)n = 3r + \frac{1}{2}r\left(\frac{M}{1+R}\right)h^2; \\ d_{i,i} = 4\left(\frac{P_r}{1+R}\right)h^2; \\ d_{i,i} = 4\left(\frac{$$

$$a_{i,i-1} = 1 - 3r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; b_{i,i-1} = 1 - 3r + \frac{1}{2}r\left(\frac{M}{1+m^2}\right)h^2; c_{i,i-1} = \left(\frac{P_r}{1+R}\right) - 3r; d_{i,i-1} = S_c - 3r + \frac{1}{2}rS_c X h^2 \quad \text{at } i = 2(1)n$$

Here, $r = k/h^2$ and h, k are mesh sizes along y, t – directions, respectively. For computational purpose the region of integration is considered as a rectangle with sides $t_{\text{max}} = 3$ and $y_{\text{max}} = 5$ where y_{max} corresponds to $(y = \infty)$, which lies very well outside the momentum, thermal and the concentration boundary layers. The Gauss elimination scheme is employed to solve the system of equations given in Eq. (30) by maintaining accuracy 0.00005. Numerical solutions for the primary and secondary fluid velocities u and w, fluid temperature $_{n}$ and fluid concentration w, a code was set up in C++ language. The mesh size h = 0.05 and k = 0.0025 was selected after comparing the results when the code was run with smaller values of k = 0.001, 0.0009 where it was noticed that the difference between these values is less than half a unity in the fourth decimal place. Also, it was found that $\left|f_i^{j+1} - f_i^{j}\right| < 10^{-5}, (f = u, w, w, w)$ at all nodal points. This designates that the method is stable. To judge the convergence of the method, computations are carried out by making small changes in the values of h and k, no significant change was noticed in the values of $u, w_{v,w}$ and w. Hence, we conclude that finite element method is stable and convergent.

The dimensionless primary and secondary skin frictions are given by

$$\ddagger_x = \frac{\partial u}{\partial y}\Big|_{y=0}$$
 and $\ddagger_z = \frac{\partial w}{\partial y}\Big|_{y=0}$

The dimensionless Nusselt and Sherwood numbers are given by

$$Nu = \frac{\partial_{u}}{\partial y}\Big|_{y=0}$$
 and $Sh = \frac{\partial W}{\partial y}\Big|_{y=0}$

Results Validation

To validate the present results, a comparison has been made by considering primary and secondary skin frictions \ddagger_x and \ddagger_z in the absence of radiation and chemical reaction with the results of Rajput and Kanaujia (2016) obtained by Laplace transform technique shown in Table 1 and 2. An excellent agreement is noticed in this comparison which validates the present numerical scheme. This justifies the correctness of the results presented in the manuscript.

Table 1. Comparison of primary skin friction between the present results and results by Rajput and Kanaujia (2016) in the absence of radiation and chemical reaction, i.e., R = 0 and x = 0.

G_r	G_m	P _r	S _c	М	т	Š <i>t</i> (degree)	t	Present results by FEM \ddagger_x	Results by Rajput and Kanaujia (2016) \ddagger_x
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10.0	10.0	0.71	2.01	2.0	0.5	30	0.2	1.1780	1.1778
20.0	10.0	0.71	2.01	2.0	0.5	30 30	0.2	1.5309	1.5307
10.0	20.0	0.71	2.01	2.0	0.5	30	0.2	3.1769	3.1768
10.0	10.0	7.00	2.01	2.0	0.5	30	0.2	1.0070	1.0063
10.0	10.0	0.71	5.00	2.0	0.5	30	0.2	0.6887	0.6887
10.0	10.0	0.71	2.01	3.0	0.5	30	0.2	0.9621	0.9621
10.0	10.0	0.71	2.01	2.0	1.0	30	0.2	1.3388	1.3387
10.0	10.0	0.71	2.01	2.0	0.5	45	0.2	1.7315	1.7314
10.0	10.0	0.71	2.01	2.0	0.5	30	0.25	1.5749	1.5744

Table 2. Comparison of secondary skin friction between the present results and results by Rajput and Kanaujia (2016) in the absence of radiation and chemical reaction, i.e., R = 0 and x = 0.

G _r	G_m	P _r	S _c	М	т	Št (degree)	t	Present results by FEM \ddagger_z	Results by Rajput and Kanaujia (2016) \ddagger_z
10.0	10.0	0.71	2.01	2.0	0.5	30	0.2	0.2149	0.2150
20.0	10.0	0.71	2.01	2.0	0.5	30	0.2	0.2210	0.2208
10.0	20.0	0.71	2.01	2.0	0.5	30	0.2	0.2560	0.2560
10.0	10.0	7.00	2.01	2.0	0.5	30	0.2	0.2108	0.2107
10.0	10.0	0.71	5.00	2.0	0.5	30	0.2	0.1975	0.1972
10.0	10.0	0.71	2.01	3.0	0.5	30	0.2	0.3065	0.3062
10.0	10.0	0.71	2.01	2.0	1.0	30	0.2	0.2790	0.2795
10.0	10.0	0.71	2.01	2.0	0.5	45	0.2	0.1988	0.1983
10.0	10.0	0.71	2.01	2.0	0.5	30	0.25	0.2490	0.2489

4. Graphical results and discussion

In order to determine the effect of physical parameters on the flow fields such as magnetic parameter M, Hall parameter m, thermal Grashof number G_r , mass Grashof number G_m , Prandtl number P_r , Schmidt number S_c , radiation parameter R, chemical reaction parameter x, phase angle St and time t, numerical computations have been carried out for primary velocity u, secondary velocity w, temperature $_{\pi}$, concentrationW, primary skin friction \ddagger_x , secondary skin friction \ddagger_z , Nusselt number N_u and Sherwood number S_h . These obtained numerical results have been presented through the graphs and Tables and then discussed.

Figure 2 illustrate the effects of thermal Grashof number G_r on the primary and secondary velocities. The thermal Grashof number G_r signifies the ratio of thermal buoyancy force to viscous hydrodynamics force. As increase in G_r tends to decrease drag forces and hence, fluid velocity increases. This implies that increase in the thermal Grashof number tends to accelerate fluid velocity in both primary and secondary flow directions. Here, the positive values of thermal Grashof number correspond to cooling of the plate. Figure 3 shows the effects of mass Grashof number G_m on the primary and secondary velocities. The mass Grashof number G_m signifies the ratio of species buoyancy force to the viscous hydrodynamic force. As mass Grashof number increases, the viscous hydrodynamic force decreases as a result momentum of the fluid increases. This implies that fluid velocity in both primary and secondary flow directions tends to increase with increasing G_m . Also, it is noticed that velocity components suddenly raise near to the plate and after this velocity components asymptotically decreases to zero as $y \rightarrow \infty$. Figure 4 represents the effect of magnetic parameter M on the primary and secondary velocities. The application of a magnetic field perpendicular to the flow direction of an electrically conducting fluid, it experiences an electric field and produces current perpendicular to both magnetic field and flow direction. The product of electric field and magnetic field creates a force which is known as Lorentz force. The direction of the Lorentz force is always opposite to the direction of the flow in the absence of applied electric field which opposes the fluid velocity. This implies that increase in magnetic parameter tends to retard the fluid velocity in the primary flow direction whereas it tends to enhance the fluid velocity in the secondary flow direction. This tendency of the magnetic field is clearly supported by the physical reality. The effects of the Hall parameter m on the primary and secondary velocities are depicted in Figure 5. It is observed that an increase in the Hall parameter tends to accelerate the fluid velocity in both primary and secondary flow directions. This situation clearly supports the fact that Hall current induces a cross-flow in the boundary layer. Figure 6 displays the effect of Prandtl number P_r on the primary and secondary velocities. As increase in P_r correspond to stronger momentum diffusivity and weaker thermal diffusivity. This implies that increase in the Prandtl number tends to decelerate fluid velocity in both primary and secondary flow direction. The influence of radiation parameter R on the primary and secondary velocities is shown in Figure 7. It is seen that both primary and secondary velocities enhance with increasing radiation parameter. This is consistent with the definition of R. Figure 8 shows the effects of Schmidt number S_c on the primary and secondary velocities. As S_c increases fluid velocity in both primary and secondary flow directions is expected to reduce since increasingly momentum is diffused at a lower rate than species. The effects of chemical reaction parameter x on the primary and secondary velocities are presented in Figure 9. It is observed that an increase in x tends to decrease the fluid velocity in both primary and secondary flow direction. Figure 10 demonstrate the effects of phase angle St on the primary and secondary flow directions. Physically, as St increase buoyancy force tends to decrease and hence, decrease the fluid momentum. The influence of time parameter t on the primary and secondary velocities is presented in Figure 9 to decrease due to increasing buoyancy effects.

Figure 12 depicts the effect of Prandtl number P_r on the fluid temperature. Prandtl number signifies the ratio of momentum to thermal diffusivities. As P_r increases thermal boundary layer thickness decreases. This implies that increase in Prandtl number tends to decrease the fluid temperature across the boundary layer. The effects of radiation parameter R on the fluid temperature are shown in Figure 13. It is observed that increase in the radiation parameter tends to enhance the fluid temperature in the boundary layer. As time progress, the fluid temperature $_{\pi}$ increases as seen in Figure 14. The effects of Schmidt number S_c on the fluid concentration W are presented in Figure 15. To be more realistic, the values of Schmidt number are chosen to represent the diffusing chemical species of most common interest like hydrogen ($S_c = 0.23$), water-vapor ($S_c = 0.64$), sulfur dioxide ($S_c = 1.20$) and naphthalene ($S_c = 2.23$). It is clear that an increase in Schmidt number tends to decrease the fluid concentration. Physically, increase in S_c decrease molecular diffusivity which results in a decrease of concentration boundary layer. Figure 16 displays the effect of chemical reaction parameter x on the fluid concentration. It is seen that increase in x tends to decrease the mass transfer. The variation of fluid concentration W with progression of time t is depicted in Figure 17. It is noticed that fluid concentration increases with increasing time t.

The numerical values of primary skin friction \ddagger_x , secondary skin friction \ddagger_z , Nusselt number N_u and Sherwood number S_h for variations in $G_r, G_m, P_r, S_c, M, m, R, X, Št$ and t are presented in Tables 3 to 5, respectively. Table 3 reveals that an increase in G_r, G_m, m, R and t tends to increase both primary and secondary skin frictions whereas an increase in P_r, S_c and X tends to decrease both primary and secondary skin frictions. Magnetic parameter M tends to decelerate primary skin friction and accelerate secondary skin friction whereas phase angle has opposite effect. Table 4 shows that an increase in P_r tends increase Nusselt number whereas it decreases with increasing R and t. It is clearly seen from Table 5, that an increase in S_c and X tends to increase Sherwood number whereas it decreases with increasing t.

Figures and Tables

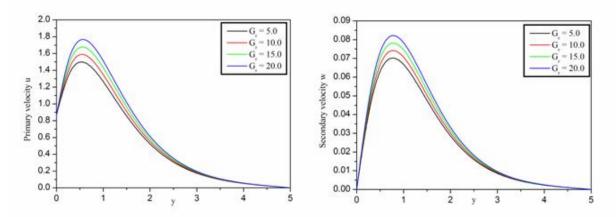


Figure 2. Primary and secondary velocities for varying G_r when $G_m = 10.0, M = 1.0, m = 0.5, P_r = 0.71, R = 1.0, M = 1.0, M$

 $S_c = 0.22, x = 0.5, \tilde{S}t = 30^0, t = 0.2.$

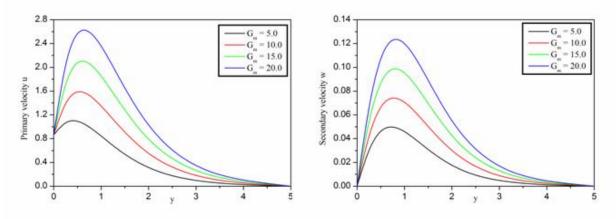


Figure 3. Primary and secondary velocities for varying G_m when $G_r = 10.0, M = 1.0, m = 0.5, P_r = 0.71, R = 1.0, S_c = 0.22, X = 0.5, Št = 30^0, t = 0.2.$

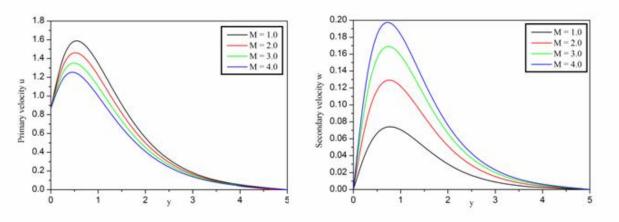


Figure 4. Primary and secondary velocities for varying *M* when $G_r = 10.0, G_m = 10.0, m = 0.5, P_r = 0.71, R = 1.0, S_c = 0.22, X = 0.5, Št = 30^0, t = 0.2.$

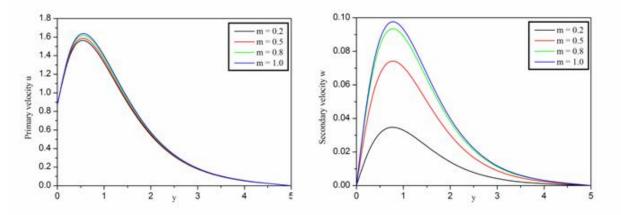


Figure 5. Primary and secondary velocities for varying *m* when $G_r = 10.0, G_m = 10.0, M = 1.0, P_r = 0.71, R = 1.0, S_c = 0.22, X = 0.5, Št = 30^0, t = 0.2.$

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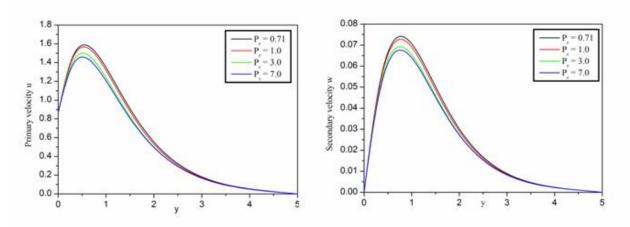


Figure 6. Primary and secondary velocities for varying P_r when $G_r = 10.0, G_m = 10.0, M = 1.0, m = 0.5, R = 1.0, S_c = 0.22, X = 0.5, Št = 30^0, t = 0.2.$

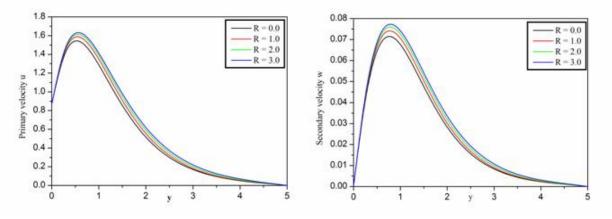


Figure 7. Primary and secondary velocities for varying R when $G_r = 10.0, G_m = 10.0, M = 1.0, m = 0.5, P_r = 0.71,$ $S_c = 0.22, x = 0.5, Št = 30^0, t = 0.2.$

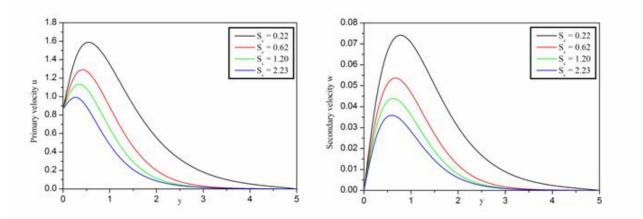


Figure 8. Primary and secondary velocities for varying S_c when $G_r = 10.0, G_m = 10.0, M = 1.0, m = 0.5, P_r = 0.71, R = 1.0, X = 0.5, Št = 30^0, t = 0.2.$

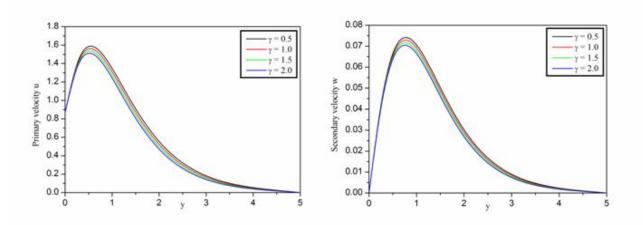


Figure 9. Primary and secondary velocities for varying x when $G_r = 10.0, G_m = 10.0, M = 1.0, m = 0.5, P_r = 0.71, R = 1.0, S_c = 0.22, Št = 30^0, t = 0.2.$

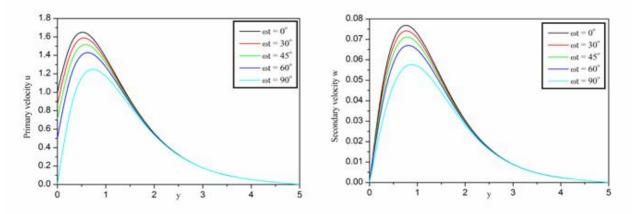


Figure 10. Primary and secondary velocities for varying Št when $G_r = 10.0, G_m = 10.0, M = 1.0, m = 0.5, P_r = 0.71, R = 1.0, S_c = 0.22, X = 0.5, t = 0.2.$

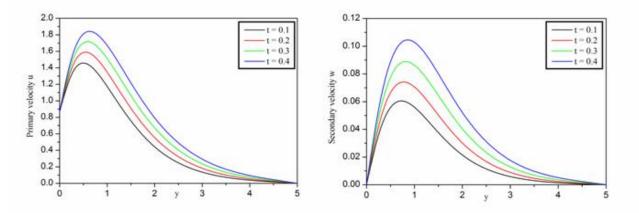


Figure 11. Primary and secondary velocities for varying t when $G_r = 10.0, G_m = 10.0, M = 1.0, m = 0.5, P_r = 0.71, R = 1.0, S_c = 0.22, X = 0.5, Št = 30^0.$

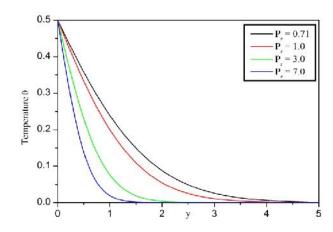


Figure 12. Temperature for varying Prandtl number P_r when R = 1.0 at t = 0.2.

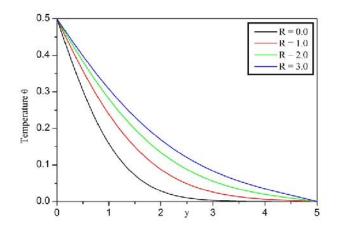


Figure 13. Temperature for varying radiation parameter *R* when $P_r = 0.71$ at t = 0.2.

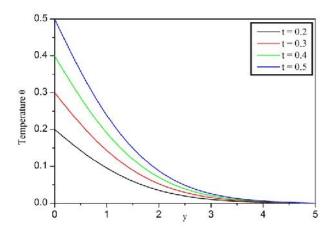


Figure 14. Temperature for varying time t when $P_r = 0.71$ and R = 1.0.

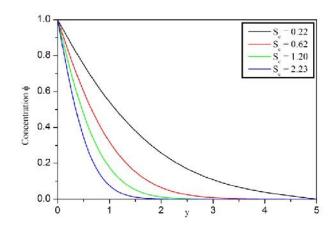


Figure 15. Concentration for varying Schmidt number S_c when x = 0.5 at t = 0.2.

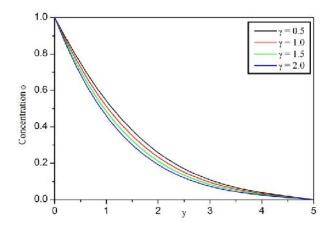


Figure 16. Concentration for varying chemical reaction parameter x when $S_c = 0.22$ at t = 0.2.

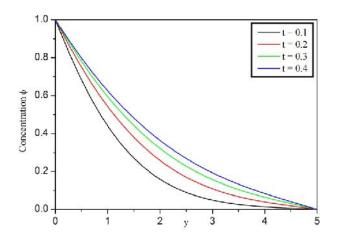


Figure 17. Concentration for varying time t when $S_c = 0.22$ and X = 0.5.

	Table 5. Numerical values of primary and secondary skill methons										
G_r	G_m	P_r	S_c	М	т	R	х	Št (Degree)	t	‡ _x	‡ _z
10.0	10.0	0.71	0.22	2.0	0.5	1.0	0.5	30	0.2	1.187770	0.182128
20.0	10.0	0.71	0.22	2.0	0.5	1.0	0.5	30	0.2	1.448654	0.199436
10.0	20.0	0.71	0.22	2.0	0.5	1.0	0.5	30	0.2	2.611304	0.282328
10.0	10.0	7.00	0.22	2.0	0.5	1.0	0.5	30	0.2	1.034078	0.169832
10.0	10.0	0.71	0.62	2.0	0.5	1.0	0.5	30	0.2	0.847760	0.148496
10.0	10.0	0.71	0.22	3.0	0.5	1.0	0.5	30	0.2	0.866006	0.438436
10.0	10.0	0.71	0.22	2.0	1.0	1.0	0.5	30	0.2	1.251342	0.237312
10.0	10.0	0.71	0.22	2.0	0.5	2.0	0.5	30	0.2	1.213240	0.184796
10.0	10.0	0.71	0.22	2.0	0.5	1.0	1.0	30	0.2	1.158930	0.180124
10.0	10.0	0.71	0.22	2.0	0.5	1.0	0.5	45	0.2	1.278982	0.170260
10.0	10.0	0.71	0.22	2.0	0.5	1.0	0.5	30	0.3	1.322450	0.207208

Table 3. Numerical values of primary and secondary skin frictions

Table 4. Numerical values of Nusselt number

P_r	R	t	N_u
0.71	1.0	0.2	0.147746
7.00	1.0	0.2	0.445450
0.71	2.0	0.2	0.120620
0.71	1.0	0.3	0.088648

Table 5. Numerical values of Sherwood number

S _c	Х	t	S_h
0.22	0.5	0.2	0.262394
0.62	0.5	0.2	0.433564
0.22	1.0	0.2	0.290562
0.22	0.5	0.3	0.229272

5. Conclusions

In this paper, the unsteady MHD mixed convective radiating and chemically reacting fluid flow past an impulsively started oscillating vertical plate with Hall current is provided. The finite element method has been applied to solve the dimensionless governing equations of the flow. It has been found that thermal and mass buoyancy force, Hall parameter, radiation parameter and time tends to accelerate both u and w whereas an increase in Prandtl number, Schmidt number, and chemical reaction rate tends to decelerate both u and w. Increase in the magnetic parameter depreciate u and reverse trend is noticed on w. These parameters have similar effect on both primary and secondary skin frictions. Phase angle causes to decrease both u and w, and opposite effect is noticed on the primary and secondary skin frictions. The fluid temperature enhanced with increment in radiation parameter and time whereas reverse trend is noticed when Prandtl number is increased and opposite effect is noticed on the Nusselt number. The fluid concentration decline with increment in Schmidt number and chemical reaction rate whereas opposite trend is observed with progression of time and opposite effect is noticed on the Sherwood number.

Nomenclature

- u' Velocity of the fluid in x' direction
- w' Velocity of the fluid in z' direction
- g Acceleration due to gravity
- s Volumetric coefficient of thermal expansion
- s^{*} Volumetric coefficient of concentration expansion
- *C*' Species concentration
- C_{∞} Concentration in the fluid away from the plate

- C_{w} Concentration at the plate
- *D* Mass diffusion
- *T* ' Temperature of the fluid
- T_{∞} Temperature of the fluid away from the plate
- T_{w} Temperature at the plate
- *k* Thermal conductivity
- € Kinematic viscosity
- ... Fluid density
- q_r Radiation heat flux
- C_p Specific heat at constant pressure
- t' Time

Acknowledgement

The author's are very grateful to the editor and reviewers for the constructive comments that led to the fruitful improvement in the manuscript.

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Received September 2019 Accepted December 2019 Final acceptance in revised form December2019