Biosorption of Nickel (II) from Aqueous Solution onto Activated Carbon Prepared from Chicken Feather

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ABSTRACT: Industrial waste water is a potential threat to human health mainly because of the presence of non-biodegradable, hazardous heavy metals. This research focuses on the use of Activated Carbon from Chicken Feathers (ACCF) in the removal of Ni (II) ions from aqueous solution. Fourier Transform Infrared (FTIR) analysis was carried out on ACCF to reveal the functional groups present which will aid adsorption. The optimization of factors such as initial metal ion concentration, pH, and contact time were investigated at ambient temperature. The optimum pH, initial metal ion concentration and contact time were therefore determined. The experimental data obtained for Ni²⁺ sorption were treated using pseudo first order and second order kinetic models. The adsorption behavior was found to follow pseudo second order kinetics. This study demonstrates the effectiveness of ACCF in the removal of Ni (II) ion from aqueous solution.

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Materials and Methods
Collection of chicken feathers: Chicken feathers were obtained from several poultry processing facilities across Zaria metropolis in Kaduna state, Nigeria. They were stored in a clean polyethylene bag before analysis was carried out.

Preparation of biosorbent (chicken feather): In order to remove some of the materials attached to the feathers, the feathers were washed severally with distilled water and detergent. It was later left in the open air for several days to get rid of odors.

Preparation of activated carbon from chicken feathers: The chicken feathers were first carbonized inside steel cups with a small hole inserted on the lids for venting gases produced during the carbonization process using a muffle furnace set at 400°C. This temperature was maintained for 1 hour, then left to cool to ambient temperature. The carbonized feathers were then impregnated with H₃PO₄ in 1:1 weight ratio and activation was then carried out using a tubular furnace set at 500°C, which was maintained for an hour.

Reagents: All chemicals, supplied by Merck Company, were of high analytical grade and stock solution of Ni (II) was prepared by dissolving appropriate amounts of Nickel chloride hexahydrate (NiCl₂·6H₂O) in deionized water and then the desired concentrations were provided by diluting the stock solution. Stock solutions of nitric acid and NaOH 0.1N were also prepared.
Experimental plan: This study investigates some factors such as the initial metal ion concentration (20, 40, 60, 80 and 100 mg/l), pH (2, 3, 5, 7, 9, 11) and contact time (10, 20, 30, 45, 60, 120 min) using batch adsorption technique. The nitric acid and NaOH 0.1N were used to adjust the pH of the solution (Rakesh and Rosy, 2017). The amount of metal ion adsorbed at equilibrium $q_e$(mg/g) was calculated by Equation:

$$q_e = \frac{V(C_i - C_f)}{S}$$

$q_e$ = Metal ion uptake capacity (mgg-1), $C_i$ = Initial concentration of metal in solution (ppm), $C_f$ = Final concentration of metal in solution (ppm), $S$ = weight of biosorbent (g), and $V$ = Solution volume (cm$^3$).

The difference between the initial metal ion concentration and final metal ion concentration was assumed to be bound to the biosorbent.

The Biosorption efficiency, A %, of the metal ion was calculated from:

$$A\% = \frac{C_0 - C_e}{C_0} \times 100$$

Where $C_0$ and $C_e$ are the initial and equilibrium metal ion concentrations (ppm), respectively (Ding et al., 2012).

RESULTS AND DISCUSSION

Characteristics of the Activated Carbon: Fourier transform infrared (FTIR) spectroscopy was used to measure the carbons of the adsorbent within the range of 400-4000 cm$^{-1}$ wave number. The FTIR technique was an important tool to identify functional groups, which are capable of adsorbing heavy metal ions. The FTIR spectrum of ACCF showed that the most prominent peaks in the spectrum originate from H-C-H asymmetric and symmetric stretching vibrations from alkanes (2924.18 to 2854.74 cm$^{-1}$). At (1635.69 cm$^{-1}$) is a stretching mode of carbonyls mainly ketones of C=O. Intense peaks in region (1512.24 to 1411.94 cm$^{-1}$) originate from the secondary Amines N-H, while stretching at (1157.33 cm$^{-1}$) for C-O come from ethers. Peaks observed at (2360.95cm$^{-1}$) originated from C≡C or C≡N.

**Effect of Initial Concentration:** Results from figure 2 showed that the removal efficiencies of Ni (II) by ACCF decreased as the initial concentration was increased from 20mg/L to 100mg/L. This is because for a fixed dose of the biomass the total available binding sites are limited, thus an increase in initial concentration from 20mg/L resulted in the exhaustion of the available binding site on the biosorbent. These results are consistent with the results obtained by Namasivayam et al., 1996. The maximum Ni (II) ion removal occurred at initial concentration of 20mg/L with percentage sorption of 96.715 %.
**Effect of pH:** The pH level of the aqueous solution is an important variable for the adsorption of metals on the adsorbent. The effect of pH on the removal of nickel ion using ACCF as an adsorbent was studied with initial pH range from 2 - 11. The relation between the initial pH of the solution and percentage removal of nickel ion is depicted in table 1. It was observed that maximum percentage sorption of nickel ions occurred at pH 9 with corresponding percentage removal of 95.99%. With increasing pH, electrostatic repulsion decreases due to reduction of positive charge density of proton on the sorption sites thus resulting in enhanced metal adsorption. Similar observations were reported by earlier researchers (Momcilović et al., 2011).

<table>
<thead>
<tr>
<th>pH</th>
<th>Percentage removal of Nickel (%)</th>
</tr>
</thead>
<tbody>
<tr>
<td>2</td>
<td>93.565</td>
</tr>
<tr>
<td>3</td>
<td>95.175</td>
</tr>
<tr>
<td>5</td>
<td>94.645</td>
</tr>
<tr>
<td>7</td>
<td>94.525</td>
</tr>
<tr>
<td>9</td>
<td>95.99</td>
</tr>
<tr>
<td>11</td>
<td>95.98</td>
</tr>
</tbody>
</table>

**Effect of Contact time:** Effect of contact time on Ni (II) removal by the sorbent is illustrated in figure 3. Rapid metal uptake in first 30 minutes was due to availability of binding sites within the sorbent, since adsorption kinetics depends on the sorbent surface area (Qader and Akhtar, 2005). Once the available binding sites were used up and clogged by metal ions, the metal uptake rate was decreased. The highest removal (99.285 %) was attained by ACCF at 60 minutes. After the adsorption equilibrium had reached on 60 minutes, a decrease in the metal uptake was observed on 120 minutes. Therefore optimum contact time for this kind of biosorbent is 60 minutes.

**Adsorption kinetics:** Adsorption kinetics was used to explain the adsorption mechanism and characteristics. Pseudo-first order and pseudo-second order kinetic models were applied to experimental data in order to investigate the kinetics of sorption of heavy metal ions onto ACCF. Kinetic study was conducted in optimum conditions determined in the preliminary experiments (initial concentration – 20 mg/dm3, temperature – 298 K and pH – 9).

**Pseudo first order model:** Pseudo first order equation or Lagergren kinetics equation (Lagergren, 1898) is widely used for the adsorption of an adsorbate from an aqueous solution and given in linearized form as presented in equation (1).

\[
\log (q_e - q_t) = \log q_e - \frac{k_1}{2.303} t \quad (1)
\]

Where \(q_t\) (mg g\(^{-1}\)) is the amount of Ni (II) adsorbed per unit mass of adsorbent at time t, \(K_1\) (L min\(^{-1}\)) is the Pseudo first order rate constant, t (min) is the time taken and \(q_e\) (mg g\(^{-1}\)) is the amount of Ni (II) adsorbed per unit mass of adsorbent at equilibrium. A correlation coefficient, \(R^2\) value close to 1 indicates an inclination towards physisorption.

![Fig.4. Pseudo first order model for Ni (II) removal using ACCF](image)

Correlation coefficient, \(R^2\) (0.9759) value indicates that the data fits into Pseudo first order kinetics model.

**Pseudo second order model:** Ho and McKay, 1991 suggested the Pseudo second order kinetic as presented in equation (2)

\[
\frac{1}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} \quad (2)
\]

Where \(K_2\) is the pseudo first order rate constant (g mg\(^{-1}\).min), \(q_e\) (mg g\(^{-1}\)) is the amount of Ni (II) adsorbed per unit mass of adsorbent and \(q_t\) is the amount of Ni (II) adsorbed per unit mass of adsorbent at time t. A correlation coefficient, \(R^2\) value close to 1 indicates an inclination towards chemisorption.
Correlation coefficient, $R^2$ (1) value suggests that the data fits into Pseudo second order kinetics model thus indicating that adsorption process occurred via chemisorption.

**Conclusion**: This study showed that ACCF could be used as an effective and efficient biosorbent for the removal of Ni (II) ions from aqueous solution. The biosorption process was affected by contact time, pH and initial concentration. Adsorption kinetics was found to follow both first and second-order rate expressions. However, the experimental data showed better fit with pseudo-second order model with higher correlation coefficients. The use of ACCF as an adsorbent clearly seems to be an economical and promising alternative over conventional methods.

**REFERENCE**


