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# Comparative Evaluation of the Adsorption of Chromium (VI) by Modified and Unmodified Mangrove Leaf Sorbents

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**ABSTRACT:** The adsorption capacity of modified (MML) and unmodified (UML) mangrove leaves sorbents on chromium (VI) was analyzed in terms of pH, adsorbent doze, chromium (VI) concentration and contact time using batch adsorption technique. Results obtained showed greater chromium (VI) adsorption on MML than UML. Adsorption capacity diagrams described for MML were higher than those of UML. The adsorption was influenced by low medium pH, low adsorbent dosage, high chromium (VI) concentration and long contact time. Adsorptive capacity decreased from 15.9 - 14.19mgg<sup>-1</sup>, for MML and 13.59 - 12.19mgg<sup>-1</sup>, for UML and from 74.99 - 9.59mgg<sup>-1</sup>, for MML and 44.89 - 5.79mgg<sup>-1</sup>, for UML as pH and adsorbent dosage were increased from (2 to 8) and (0.25 to 2g); but increased from 5.09 - 46.19mgg<sup>-1</sup>, for UML and 1.89 - 25.59mgg<sup>-1</sup>, for UML and from 26609.0 - 38719.0mgg<sup>-1</sup>, for MML and 28869.0 - 35089.0mgg<sup>-1</sup>, for UML as concentration of chromium (VI) and time of contact increased from (10 to 100ppm) and (30 to 240minutes), respectively. Isotherm studies reveal that experimental data for MML and UML fitted on Freundlich adsorption ( $R^2 \ge 0.93$ ). Kinetic data analyses, with ( $R^2 \ge 0.962$ ) on pseudo-second order model, suggest chemisorption process for both sorbents. These results suggest the extract of mangrove leaves material after acid modification can be used as biosorbent for chromium (VI) removal in aqueous solution.

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Chromium is one of the most common heavy metal pollutants released into the environment during chrome-plating, leather tanning, wood preservation and mining operations (Nordiana et al., 2013). It has multiple oxidation numbers ranging from -2 to +6. The +3 and +6 states are more prevalent but the latter is more soluble and toxic in aqueous environment (Sathish, et al., 2015). Chromium has been reported to be carcinogenic and can cause nasal, kidney and liver damage, asthma, ulcer and skin irritation when found above the tolerance level (Stout et al., 2009). Many researchers (Nameni et al., 2008; Olayinka et al., 2009; Abdullahi et al., 2012; Ofudje et al., 2016; Timbo et al., 2017) have focused on adsorption techniques, especially the use of agricultural waste materials for the removal of heavy metals from aqueous solutions. Studies on the use of modified and unmodified plant materials have been reported (Rozaini et al., 2010; Ofudje et al., 2014; Sathish et al., 2015).

Mangrove (*Rhizophora mangle*), a marine coastal plant, is abundantly found in the southern region of Nigeria. The stem of the plant is harvested for use as fire wood and for making charcoal by the inhabitants of the local communities while the leaves and roots are left as wastes. Conversion of these to valuable adsorbents would not only be economical but help reduce the waste disposal problems. According to Vazqueze *et al.* (2002) and Sathish, *et al.* (2015) these leaves contain polyphenolic compounds which under appropriate conditions are capable of adsorbing metal ion from solutions (sathish *et al.*, 2015). In this work, the adsorption efficiencies of modified (MML) and unmodified (UML) leaves extracts sorbents in taking up chromium (VI) from aqueous solution was investigated by batch adsorption method. The objective of this paper was to evaluate and report the adsorption capacities of modified and unmodified mangrove leaf sorbents.

Materials and Methods: Analytical grade chemicals (potassium dichromate, sodium hydroxide, hydrochloric acid, sulfuric acid, sodium bicarbonate and nitric acid) were used without further purification. Other materials used were pocket size HANNA pH Meter (model H196107), phenonm world SEM-PRO (model X800-07334), Atomic Absorption Spectrophotometer (Agilent MP-AES 42100), mechanical grinder, 500µm test sieve and Stuart orbital shaker.

Sample Preparation: Mangrove (Rhizophora) leaves were collected from swamp forest near Bakana, a

riverine community in Degema Local Government Area of Rivers State, Nigeria. The leaves were thoroughly washed with deionized water to remove dirt, soil and other soluble particles, sun-dried for 5 days, crushed with mechanical grinder to obtain dry powder and then sieved using test sieve of 500µm particle size. Modification was done according to the method described by Nordiana et al., 2013. 30g of the desired particle size  $(500\mu m)$  was treated with 50ml of 0.5M Sulfuric acid solution and kept in an oven for 24hrs, then soaked in de-ionized water until the pH of the solution stabilized. 50ml of 0.5M sodium bicarbonate was added to the solution. After 1hr, it was washed with de-ionized water until all residual acid was finally removed. The sample was oven dried for 5hrs at 110°C until constant weight, then cooled and stored in a tightly covered container for further studies. Stock solution (1000ppm) of chromium (VI) was prepared by dissolving 2.828g of potassium dichromate (K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub>) in 1 liter of deionized water. Working solutions (10ppm, 20ppm, 40ppm, 60ppm and 100ppm) were prepared from the stock by serial dilution. Surface morphology of the samples at the desired particle size was analyzed using Scanning Electron Microscope.

#### METHODS AND METHODS

Batch Adsorption Experiment: For both the modified and unmodified mangrove leaves sorbents, the effect of variations in pH (2 - 9), adsorbent doze (0.25 - 2g) and chromium (VI) concentrations (10 - 100ppm) on the adsorption of chromium (VI) were carried out. The contact time was varied at 30 minutes intervals between 30 and 240 minutes, by determining residual chromium (VI) at the predetermined time intervals. Adjustment of pH was actualized by adding aqueous solutions of 0.1M HCl or 0.1M NaOH. In each of these experiments, 20ml portion of chromium (VI) solution was measured and the resulting mixture equilibrated on an orbital shaker set at a speed of 150rpm. The content of each beaker was filtered into a conical flask through Whatman No. 1 filter paper and the residual chromium (VI) concentration in the filtrate determined using AAS.

*Adsorption Isotherm*: Adsorption isotherm studies were carried out with initial concentrations of 10, 20, 40, 60 and 100ppm at pH of 2 using 0.2g of the adsorbent. Langmuir and Freundlich isotherm models were employed to interpret the adsorption process (equations 1 and 2 respectively).

$$\frac{C_e}{q_e} = \frac{K_l}{q_{max}} + \frac{1}{q_{max}} C_e$$
(1)  
$$\log q_e = \log K_f + \frac{1}{n} \log C_e$$
(2)

where  $q_{max}$  is the maximum adsorption at monolayer (mg/g),  $C_e$  is the equilibrium concentration of the adsorbate ion in solution,  $q_e$  is the amount of ion adsorbed per unit weight of the adsorbent,  $K_L$  is the Langmuir constant related to the affinity of binding sites,  $K_f$  and n are called freundlich constants.  $K_f$  defines the relative adsorption capacity while n indicates the intensity of the adsorption.

The percentage chromium (VI) removed by mangrove leaves was evaluated from the difference between the initial ( $C_o$ ) and final ( $C_f$ ) concentrations as shown in equation 3. The amount of Chromium (VI) ion adsorbed was calculated using equation 4.

% Removal = 
$$\frac{(C_0 - C_f)100}{C_0}$$
 (3)

$$q_e = \frac{(C_o - C_f)V}{m} \tag{4}$$

Where  $q_e$  is the equilibrium adsorption capacity (mg/g),  $C_0$  and  $C_f$  are the initial and final concentrations of chromium (VI) (mg/l), V is the volume of solution (l) and m is the mass of the adsorbent used (g).

*Kinetic Studies:* To investigate the kinetic properties of the adsorption, 0.2g of the adsorbent was added to 20ml of 60ppm chromium (VI) solution and agitated for time intervals of 30, 60, 90, 120, 150, 180, 210 and 240mins. The kinetics process was analyzed using the Pseudo-first order (equation 5) and pseudo-second order (equation 6) adsorption models by Lagergren (Ngugi. 2015).

$$\log(q_e - q_t) = \log q_e - (\frac{\kappa_1}{2.303})t \quad (5)$$
  
$$\frac{t}{q_t} = \frac{1}{\kappa_2 q_e^2} + \frac{1}{q_e}t \quad (6)$$

In equations 5 and 6,  $q_e$  and  $q_t$  represent the amount of chromium (VI) adsorbed at equilibrium and at a given time, t. K<sub>1</sub> and K<sub>2</sub> are the rate constants of the pseudo-first order and pseudo-second order adsorption processes, respectively.

#### **RESULTS AND DISCUSSION**

Surface Morphology: Images of modified and unmodified mangrove leaves samples were taken so as to observe possible changes on the surface if any. The SEM micrographs are presented in Figure 1. Both images were taken at 200 $\mu$ m. Figure 1A appears to be more porous and have wider surface area than UML (Figure 1B). Thus, MML has wider surface feasibility to adsorb chromium (VI) ions than UML.

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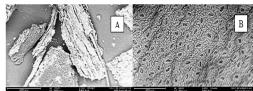


Fig 1. SEM images of (A) MML and (B) UML.

Effect of pH: The adsorption capacities of 0.2g MML and UML as a function of pH are presented in Fig. 2. The results show that the adsorption of chromium (VI) by both MML and UML decreased with the pH of the medium. Similar observation has also been made elsewhere (Sathish, et al., 2015). High adsorption capacity at low pH was attributed to strong electrostatic attraction between the adsorbent surface and the adsorbate. Adsorption of ions by biomaterials depends largely on the presence of active sites, nature of ion and pH of the medium under consideration. It is generally known that in low pH, the adsorbent surface become positive while in alkaline medium (high pH), adsorbent surface becomes negative. Chromium (VI), the hexavalent chromium ion, exists predominately in solution and in acidic medium as chromate ion (HCrO<sub>4</sub><sup>-</sup>) and thus possesses an anionic atmosphere which is negative (Olayinka et al., 2009) and so was adsorbed more in acidic medium by electrostatic attraction on the adsorbent surface. At higher solution pH, electrostatic repulsion reduced chromium (VI) adsorption, thus adsorption capacity decreased.

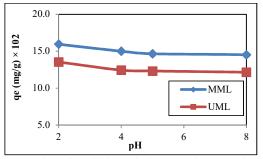


Fig 2: Plots of equilibrium adsorbent capacity,  $q_e$  (mg/g) as a function of solution pH for the adsorption capacity  $q_e$  (mg/g) as a function of Solution pH for the adsorption of Chromium (VI) by Mangrove leaves.

*Effect of Adsorbent Doze:* Figure 3 shows the inverse relationship between the adsorption capacities of modified and unmodified mangrove leaves and adsorbent doze. Similar observation has been made by Sathish, *et al.*, (2015). The researchers did not provide reasonable explanation for the inverse relationship. It is known that increase in adsorbent doze results in larger surface area and more active sites for adsorption. Thus increase in adsorption capacity with dosage was expected. The decrease in adsorption

capacity observed in this study is possibly due to increasing unsaturation caused by overcrowding of particles as the adsorbent doze increased.

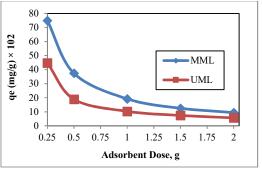
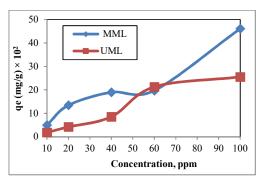


Fig 3: The adsorption capacity,  $q_e (mg/g)$  as a function of adsorbent doze (g) for 100ppm solution of chromium (VI)

Effect of Chromium (VI) ion Concentration: The adsorption capacities of modified and unmodified mangrove leaves on chromium (VI) are presented in Figure 4. The results indicate that the adsorption of chromium (VI) ion by MML and UML is directly proportional to the concentration of chromium (VI) ion. It is also observed that the adsorption capacity of MML was greater than that of UML. The increase in adsorption capacity observed can be attributed to the fact that the binding site was not saturated and so could probably bind more chromium (VI) if a higher initial concentration was used. Figure 4 reveals increase in adsorption capacity with concentration of the adsorbate with larger values of qe for MML than UML. This agrees with the SEM surface analysis (Figure 1) that indicates that MML has wider surface feasibility and more binding sites than UML.



**Fig 4**: plot of Adsorption capacity of Mangrove leaves as a function of initial Chromium (VI) concentration [pH = 2, adsorbent doze = 0.25g]

*Effect of Contact Time:* Adsorption capacities of MML and UML are displayed as a function of time of contact (Figure 5). The results (Figure 5) indicate that the adsorption capacity of both MML and UML increased with increase in contact time even after the

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attainment of equilibrium at 210 minutes, from 2660 to 3991mg/g, for MML and from 2886 to 3775mg/g, for UML. The increase may be due to long time of contact and also the availability of the vacant binding site on the adsorbents. The results suggest that the equilibrium time is dependent on the nature of the adsorbent. The higher values of qe obtained for MML than UML supports the results of Figure 4.

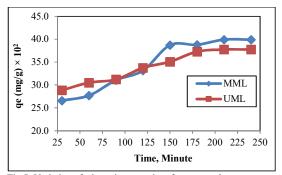


Fig 5: Variation of adsorption capacity of mangrove leaves on chromium (VI) as a function of time (minutes) [pH = 2, adsorbent doze = 0.25g, chromium (VI) conc. = 100ppm]

Adsorption Isotherm: Adsorption isotherm describes the equilibrium relationship between the adsorbate in the solution and the adsorbate on the adsorbent at constant temperature (Ali Riza *et al.*, 2007). Models such as those of Langmuir (equation 1) and Freundlich (equation 2) are widely employed to describe experimental sorption data (Cookey *et al.*, 2018). Langmuir parameters ( $q_{max}$  and  $K_1$ ) were calculated from the slope and intercept of the linear plot of Ce/qe versus Ce as depicted in equation 1. Similarly, Freundlich parameters (n, and  $K_f$ ) were obtained from the slope and intercept of the linear plot of log qe versus log Ce (equation 4). Their application is based on best-fit correlation coefficient ( $\mathbb{R}^2$ ) values. Good  $\mathbb{R}^2$  values of 0.96, for MML and 0.93, for UML, indicate that the isotherm data contained in Table 1 are in conformity with Freundlich model, suggesting heterogeneous adsorption on surfaces of MML and UML. Favourable adsorption process occurs if n lies between 1 and 10 (Timbo, *et al.*, 2017). Hence, with n value of 1.116, for MML and 0.63, for UML, the results indicate that adsorption of chromium (VI) was more favoured on the surface of MML than UML. As may be seen, poor  $\mathbb{R}^2$  values (0.38 and 0.76) and other Langmuir parameters in Table 1 indicate non-conformity with the model.

Adsorption Kinetics: Kinetic parameters for the adsorption of chromium (VI) from aqueous solution were studied using the pseudo first (Equation 5) and second order (Equation 6) models. The Pseudo first order kinetic parameters were calculated by plotting graph of log  $(q_e - q_t)$  versus t (time). The values of Pseudo-second order rate constant k<sub>2</sub> and equilibrium adsorption capacity qe were calculated from the intercept and slope of a plot of t/qt versus t. These parameters have been evaluated for MML and UML and compared in Table 2. With pseudo-second order qe and K<sub>2</sub> values of 5000mg/g and 6.66  $\times$  10<sup>-</sup> <sup>6</sup>g/mg/minute computed for MML, and 3333mg/g and 3.103 x10<sup>-5</sup>g/mg/minute for UML, the results suggest that adsorption of chromium (VI) on the biomass occurred by chemical means and MML was a better adsorbent than UML. This is also in conformity with the R<sup>2</sup> values of 0.9959, for MML and 0.9623, for UML. Table 2 also indicates good fit ( $R^2 = 0.94$ ) for UML in the pseudo-first order model. However, the evaluated  $q_e$  and  $K_1$  values (1321mg/g and 0.0099) are relatively low.

	Langmuir			Freundlich		
	K <sub>L</sub> (l/mg)	Q <sub>max</sub> (mg/g)	$\mathbf{R}^2$	K <sub>f</sub> (mg/g)	n	$\mathbf{R}^2$
MML	178.89	1111	0.383	74.67	1.116	0.9627
UML	-70.00	-1250	0.761	5.131	0.630	0.931

**Table 1**: Isotherm Parameters for the adsorption of Chromium (VI) on MML and UML surfaces

	Table 2: Kinetic Parameters of the adsorption of Chromium (VI) on MML and UML surfaces									
	Pseudo-first order			Pseudo-Second order						
	q <sub>e</sub> (mg/g)	K <sub>1</sub> (mins <sup>-1</sup> )	$\mathbf{R}^2$	qe (mg/g)	K <sub>2</sub> (g/mg/mins)	$\mathbf{R}^2$				
MML	3286	-0.0179	0.7563	5000	6.66 x 10 <sup>-6</sup>	0.9959				
UML	1321	0.0099	0.94	3333	3.103 x10 <sup>-5</sup>	0.9623				

*Conclusion*: This study has compared the adsorption of chromium (VI) on modified and unmodified mangrove leaves sorbents in aqueous medium as functions of pH, adsorbent doze, initial concentration of chromium (VI) and contact time in aqueous medium using batch adsorption technique. It was found that MML exhibited higher adsorption capacity than UML. The adsorption was found to be more effective at low pH and adsorbent dosage, high chromium (VI) concentration and in longer contact time. Isotherm data analyses suggest heterogeneous adsorption for both adsorbents. The adsorption process is chemical in

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nature, according to kinetic studies. The overall results indicate that mangrove leaves, from an abundantly available plant, have great potential to adsorb chromium (VI) from aqueous solution.

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