

EVALUATION OF RTD AND THERMOCOUPLE FOR PID TEMPERATURE CONTROL IN DISTRIBUTED CONTROL SYSTEM LABORATORY

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ABSTRACT

Temperature process control is an integral element in the syllabus of control engineering. Generally, industrial processes can be simulated via proportional-integral-derivative (PID) controller and various tunings methods. This paper proposes a process control laboratory and sequence of experiments in basic temperature control process. The experiments are performed on temperature control plant using resistor temperature detector (RTD) and thermocouple in a distributed control system laboratory. Five PID experiments are conducted. These include optimum tuning of the controller using Ziegler-Nichols process reaction-curve method, ultimate gain and response of various proportional band, integral band and derivative band values to the temperature control. PID tuning is observed and analyzed for the respective RTD and thermocouple sensors.

Keywords: RTD; thermocouple; distributed control system; temperature process control.

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1. INTRODUCTION

Experimental learning is an instructional approach that provides direct understanding on the knowledge being taught. The pedagogy involves self-action and self-determination, as well as hands-on activity. In essence, learning is a process where knowledge is being created through experience [1-2]. Reflective observations have known to benefit in the formation of new knowledge. By adopting experiential learning approach, students will be exposed to new experiences through projects that have connotations in the preceding courses. Hence, students are required to reflect on their existing knowledge to solve the given problems [3]. Innovative pedagogies have since been developed to improve the delivery approach[4-5]. Problem-based learning (PBL) is one method that has been designed to provide a focused, dynamic and problem-oriented approach in learning. The technique has been implemented in a wide range of academic specializations [6].

Generally, students are required to be physically involved in experiments and relate observations with the established theories. The reflections then allow crystallization of core knowledge within their mind [3]. Any discrepancies that occur during experiments or problems encountered will trigger the relevant brain segments to find a solution. Often, such tasks are best delegated in groups as there will usually be more than one answer for any encountered problem. The approach has proven to enhance students' understanding on the subject matter [4]. Consequently, these serves a bridge between the theories learned in formal education and critical thinking skills that are required in the industry [7-8]. PBL can be implemented in various formats such as mini-projects that are embedded in specific courses and open-ended experiments that mimic industry-related problems. Apart from practical knowledge and critical thinking skills, the pedagogy also improves the ability of students to work in teams.

Recently, academic activities in control engineering have been redesigned to match the requirements of manufacturing industries. Temperature control is one of the simpler forms of industrial process that can be simulated using PID controller in the laboratory [9-10]. The classical controller is still widely implemented to study characteristics and new tuning methods [11-12]. The temperature will depend on the adjustment of control variables, so that it conforms to the stability and other process requirements. To obtain a reliable output

however, the controller must be well-tuned. A common approach to achieve optimum response is by using Ziegler-Nichols tuning method. The technique controls air temperature by adopting the tangent method in its open-loop test. Thus far, the Ziegler-Nichols approach has demonstrated the best rise time, settling time, and smallest integral absolute error [13]. Therefore, the study evaluates the temperature control [20] process of PID tuning module in the Distributed Control System (DCS) laboratory.

2. OVEN TEMPERATURE SYSTEM

Students are introduced to simple but real-time temperature control using PBL approach. Fig. 1 shows the temperature control [21] plant at the Faculty of Electrical Engineering, Universiti Teknologi MARA. The plant is developed by Yokogawa for engineering education purposes and can be controlled using DCS technique. Temperature in the chamber is measured by RTD and thermocouple. Information from the sensors is used by the single-loop system to control the heater via continuous output current control [13].



Fig.1. Temperature control plant [13]

3. PID CONTROL

Ziegler-Nichols method is used in the tuning process. Adjustments to the proportional, integral and derivative elements will influence the performance of PID controller [14]. Two

widely used methods are closed-loop and open-loop tuning approaches. In the closed-loop method, the controller is tuned in the automatic state; operating in closed-loop configuration. Fig. 2 shows the typical ultimate gain curve tuning for closed-loop response [15].

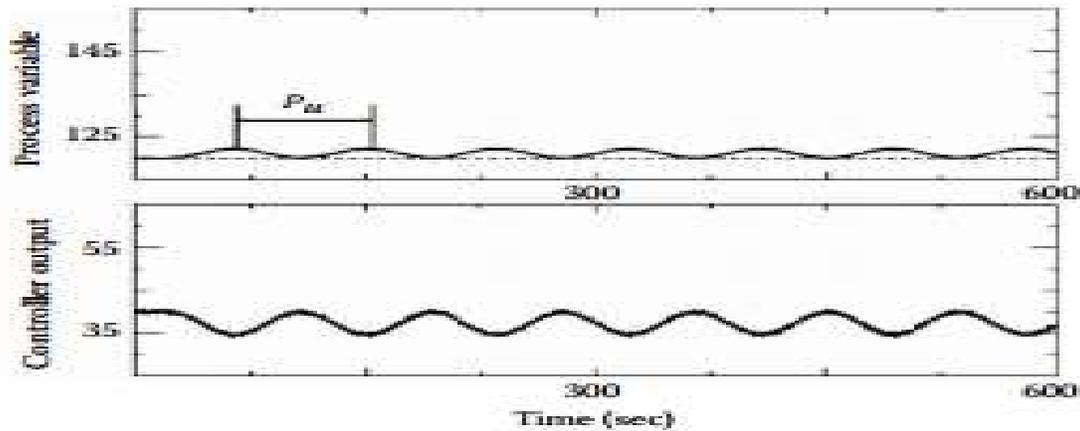


Fig.2.Ultimate gain curvetuning for closed-loop response [16]

Meanwhile, the open-loop technique is a method that tunes the controller in manual state; the plant is operating in open-loop configuration. Fig. 3 shows the typical process reaction curve open-loop response [15].

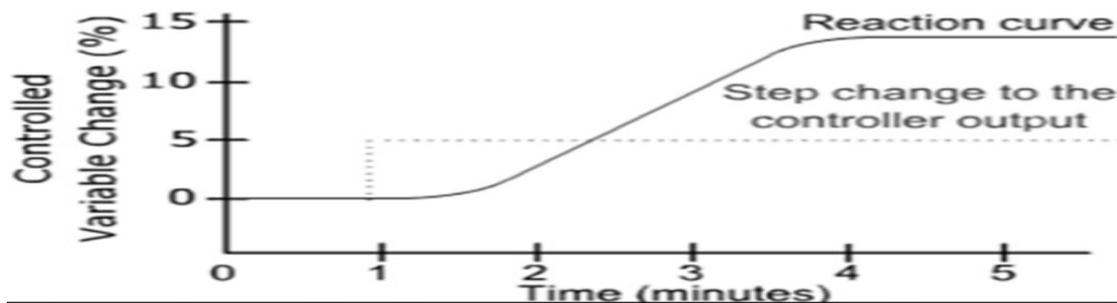


Fig.3.Process reaction curve for open-loop response [17]

4. METHODOLOGY

4.1.RTD and Thermocouple

RTD and thermocouple are commonly used sensors to measure temperature for monitoring and control purposes. In this study, the two sensors used by the Yokogawa plant is thermocouple type J and PT100 RTD sensors.

4.2.PID

Table 1 and Table 2 each show the optimization of process reaction curve and ultimate gain curve. Both optimization processes are performed using Ziegler-Nichols tuning method. RR, T_d , T_I , T_D , PU and PBU, each denotes reaction rate, dead time, integral time, derivative time, period of ultimate gain and proportional band ultimate gain.

Table 1. Optimization of process reaction curve using Ziegler-Nichols method [18]

Controller Mode	Proportional Band (%)	Integral Time, T_I (s)	Derivative Time, T_D (s)
P	100 x RR x T_d	Off	Off
PI	111.1 x RR x T_d	3.33 x T_d	Off
PID	83.3 x RR x T_d	2.0 x T_d	0.5 x PU

Table 2. Optimization of ultimate gain curve using Ziegler-Nichols method [18]

Controller Mode	Proportional Band (%)	Integral Time, T_I (s)	Derivative Time, T_D (s)
P	2 x PBU	Off	Off
PI	2.2 x PBU	0.83 x PU	Off
PID	1.7 x PBU	0.5 x PU	0.125 x PU

5. EXPERIMENTS AND TUNING

5.1.Open Reaction Curve Determination with Continuous Output Current Control

Initially, a simple open-loop test is performed to determine the value of T_d , time constant (T_c) and gain (K_p) using tangent method. The desired temperature is set to 45°C and the response is analyzed. Then, the values for proportional band, integral time and derivative time are calculated using Ziegler-Nichols tuning method shown in Table 1. The experiment is conducted with set point change function of DCS from manual to automatic mode. In closed-loop configuration, the performance is evaluated in terms of dynamic response.

5.2.Ultimate Gain Method Using Continuous Current Control Output

In the next experiment, the desired temperature is also set to 45°C. The PID values are each set to $P = 10$, $I = 1$ and $D = 0$. The set point value is then changed to 55°C and the response is

analyzed to determine PU and PBU. The values of proportional band, T_I and T_D are each calculated using the equations shown in Table 2.

5.3. Effect of Different Proportional Band Values

Similar temperature setting of 45°C is used for the subsequent experiment. The controller is already in automatic mode but with different values of proportional bands in the PID settings. The response is observed to determine settling time (T_s), rise time (T_r), percentage overshoot (%OS), steady-state error (%SSE), oscillation and decay ratio. The experiment is repeated for different proportional band values and changes in response are compared.

5.4. Effect of Different Integral and Derivative Time Values

The study adopts a similar method as the preceding experiment. Observations however, focus on comparing the effect of changes in integral and derivative values on the response.

6. RESULTS AND DISCUSSION

6.1. Open Reaction Curve: Tangent Method

Fig. 4 and Fig.5 each show the resultant process reaction curve for the open-loop test. A step change of manipulated variable (MV) changed from 30% to 45%. Initially, the steady state temperature is 36.1°C. Then, it requires between 20 to 30 minutes to reach a new steady state for both RTD and thermocouple sensors. Using the tangent method, values of T_c , RR and T_d are then calculated using tangent method. Fig. 4 shows the output reaction curve for RTD sensor.

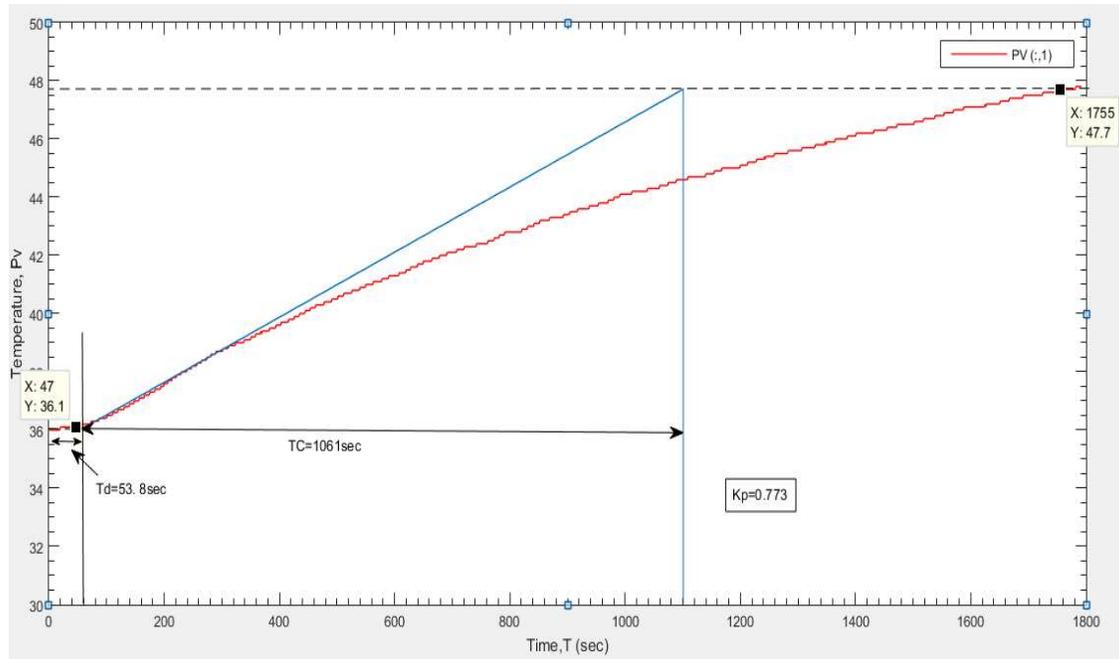


Fig.4. Process reaction curve with RTD input

The RR for RTD is determined by the following computation.

$$T_c = 138.0 \text{ mm} \times \frac{200 \text{ s}}{26.0 \text{ mm}} = 1061 \text{ s}$$

$$RR = \frac{\Delta PV / T_c}{\Delta MV} = \frac{11.6 / 1061}{15} = 0.0007 \text{ s}^{-1}$$

$$T_d = 7.0 \text{ mm} \times \frac{200 \text{ s}}{26.0 \text{ mm}} = 53.8 \text{ s}$$

Meanwhile, the output reaction curve for thermocouple sensor is shown in Fig. 5.

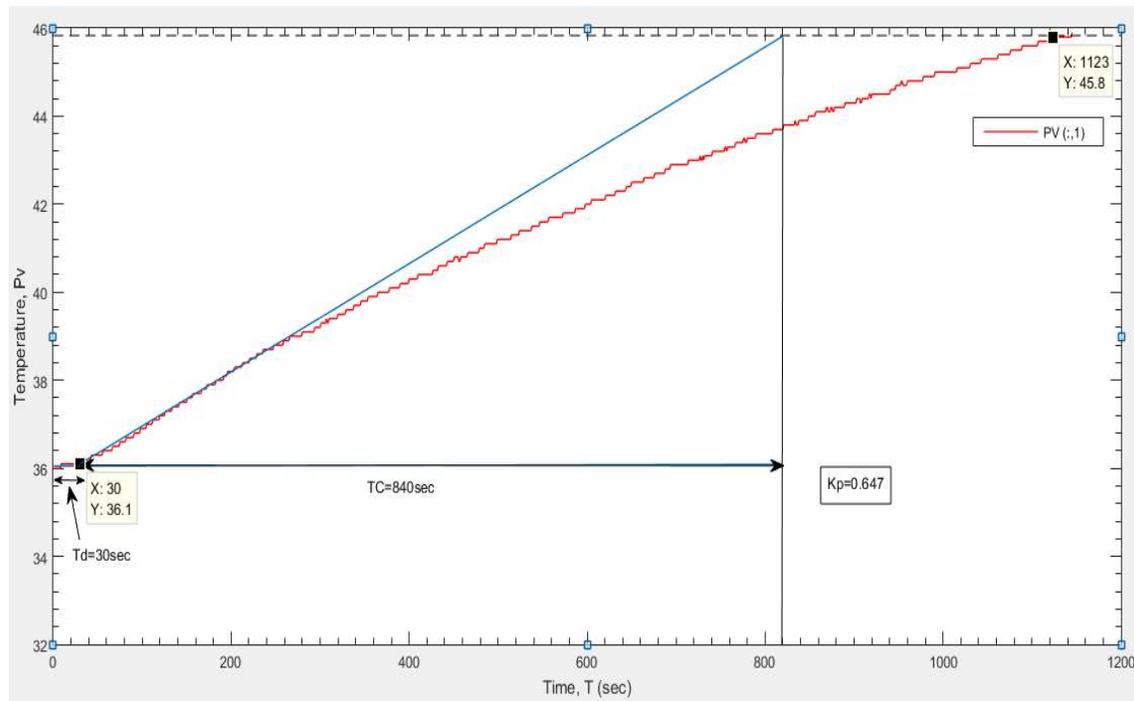


Fig.5. Process reaction curve with thermocouple input

The RR for thermocouple sensor is determined by the following computation.

$$T_c = 168.0 \text{ mm} \times \frac{200 \text{ s}}{40.0 \text{ mm}} = 840 \text{ s}$$

$$RR = \frac{\Delta PV / T_c}{\Delta MV} = \frac{9.7 / 840}{15} = 0.0007 \text{ s}^{-1}$$

$$T_d = 6.0 \text{ mm} \times \frac{200 \text{ s}}{40.0 \text{ mm}} = 30.0 \text{ s}$$

6.2. Ultimate Gain Curve Determination: Process Identification Method

Ultimate gain curve tuning is a trial-and error method that is still widely adopted [18]. Parameters for PBU and PU are determined from the output of the oscillation response shown in Fig. 6 and Fig. 7.

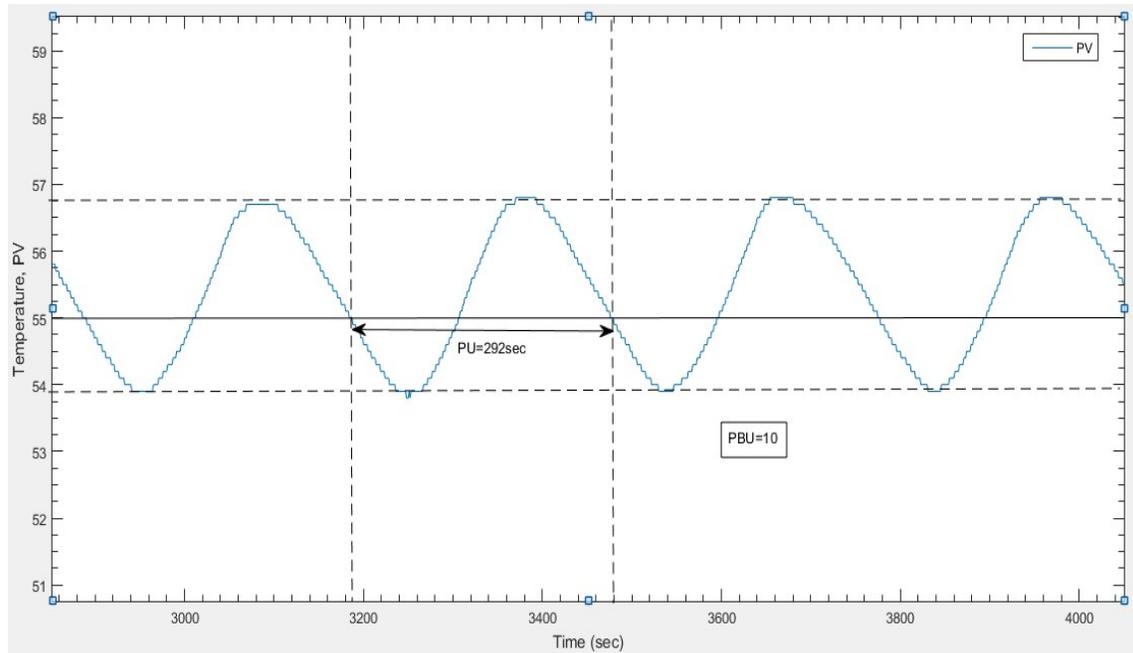


Fig.6. Ultimate gain curve with RTD input

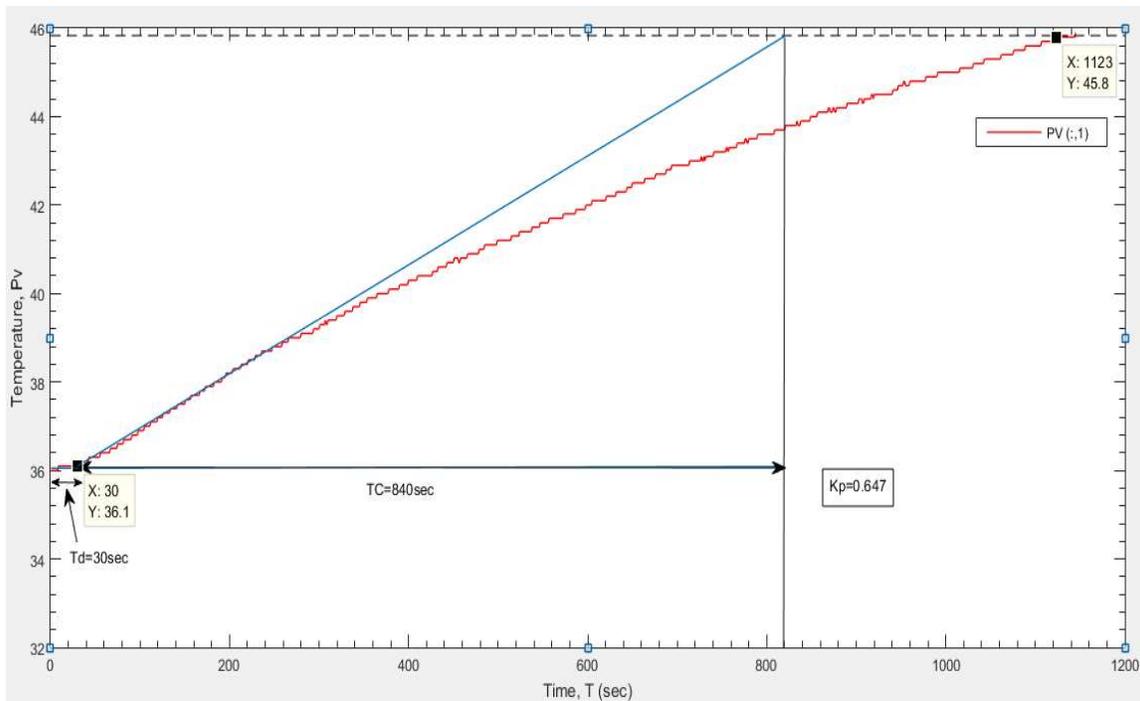


Fig.7. Ultimate gain curve with thermocouple input

6.3.PID Tuning

Values of the proportional band, T_I and T_D are determined by parameters calculated in section 6.1. Table 4 and Table 5 each summarizes the optimized values for the reaction curves for RTD and thermocouple sensors based on Ziegler-Nichols tuning method.

Table 4. Optimization of process reaction curve with RTD input

Controller Mode	Proportional Band (%)	Integral Time, T_I (s)	Derivative Time, T_D (s)
P	3.766	Off	Off
PI	4.184	170.154	Off
PID	3.137	107.6	26.9

Table 5. Optimization of process reaction curve with thermocouple input

Controller Mode	Proportional Band (%)	Integral Time, T_I (s)	Derivative Time, T_D (s)
P	2.1	Off	Off
PI	2.333	99.9	Off
PID	1.7489	60	15

Meanwhile, Fig. 8 and Fig. 9 each show the output characteristics in terms of dynamic responses which include peak time (T_p), %OS, %SSE, T_r and T_s .

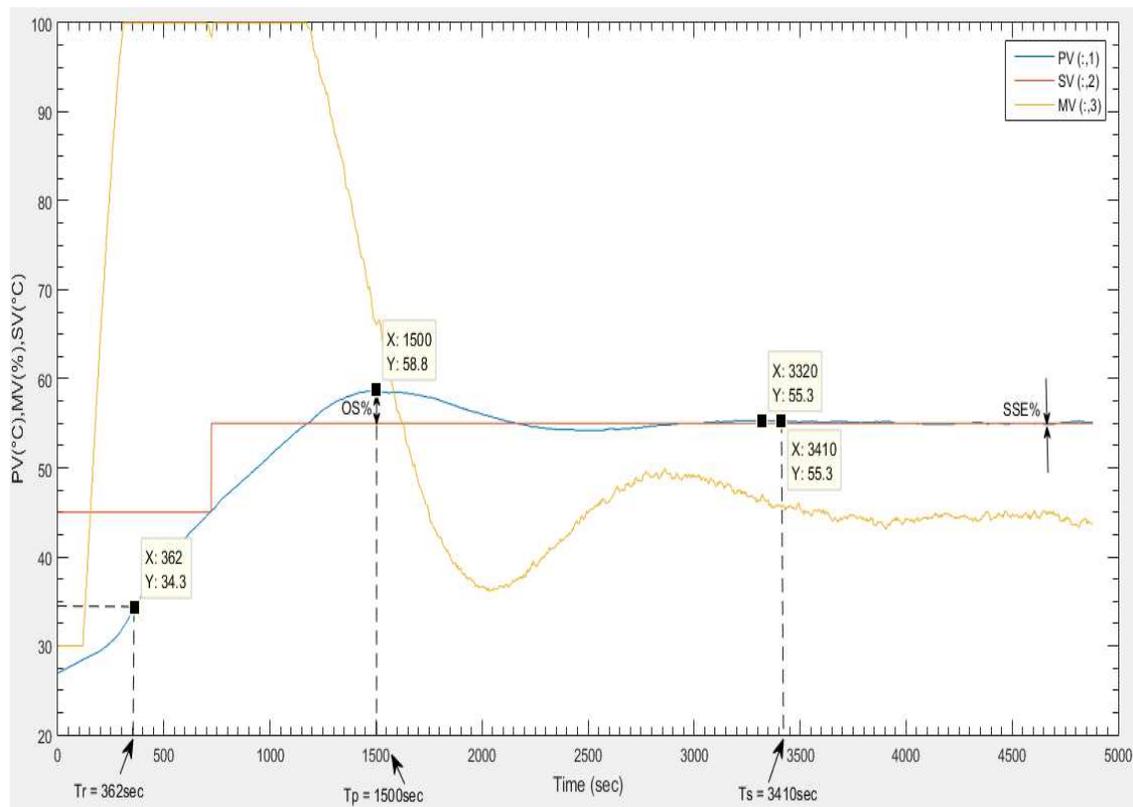


Fig.8. Closed-loop response of PID tuning with RTD input

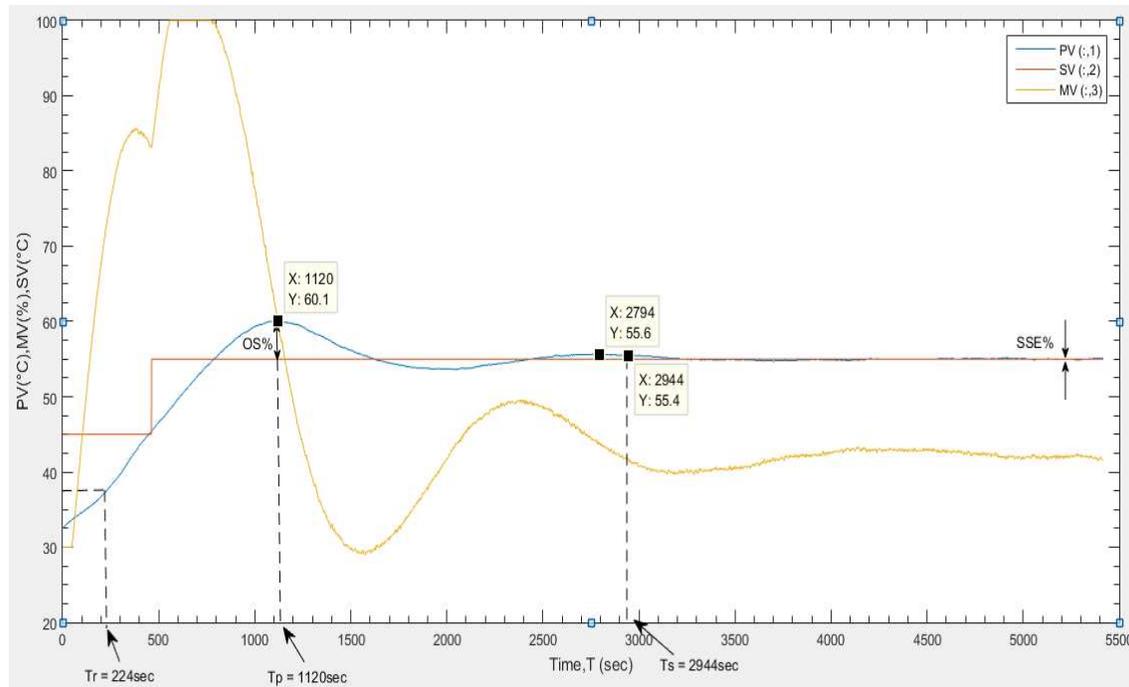


Fig.9. Closed-loop response of PID tuning with thermocouple input

The values of PBU and PU are determined via process identification method. The parameters are then used to calculate the proportional band, TI and TD. Subsequently, the optimized ultimate gain curve for RTD and thermocouple inputs are each shown in Table 6 and Table 7. The parameters are tuned using Ziegler-Nichols method.

Table 6. Optimization of ultimate gain curve with RTD input

Controller Mode	Proportional Band (%)	Integral Time, T_I (s)	Derivative Time, T_D (s)
P	20	Off	Off
PI	22	534.36	Off
PID	17	146	36.5

Table 7. Optimization of ultimate gain curve with thermocouple input

Controller Mode	Proportional Band (%)	Integral Time, T_I (s)	Derivative Time, T_D (s)
P	30	Off	Off
PI	33	267.26	Off
PID	25.5	161	40.25

Meanwhile, the dynamic responses for all the process for RTD and thermocouple sensors are shown in Fig. 10 and Fig. 11 respectively.

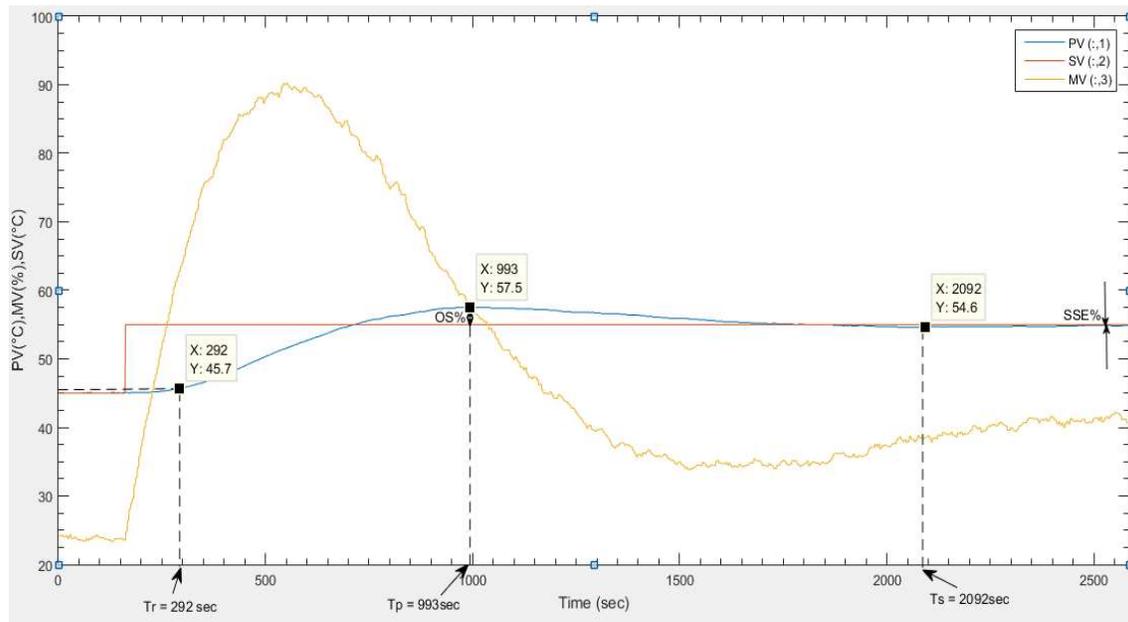


Fig.10. Output response of PID tuning with RTD input

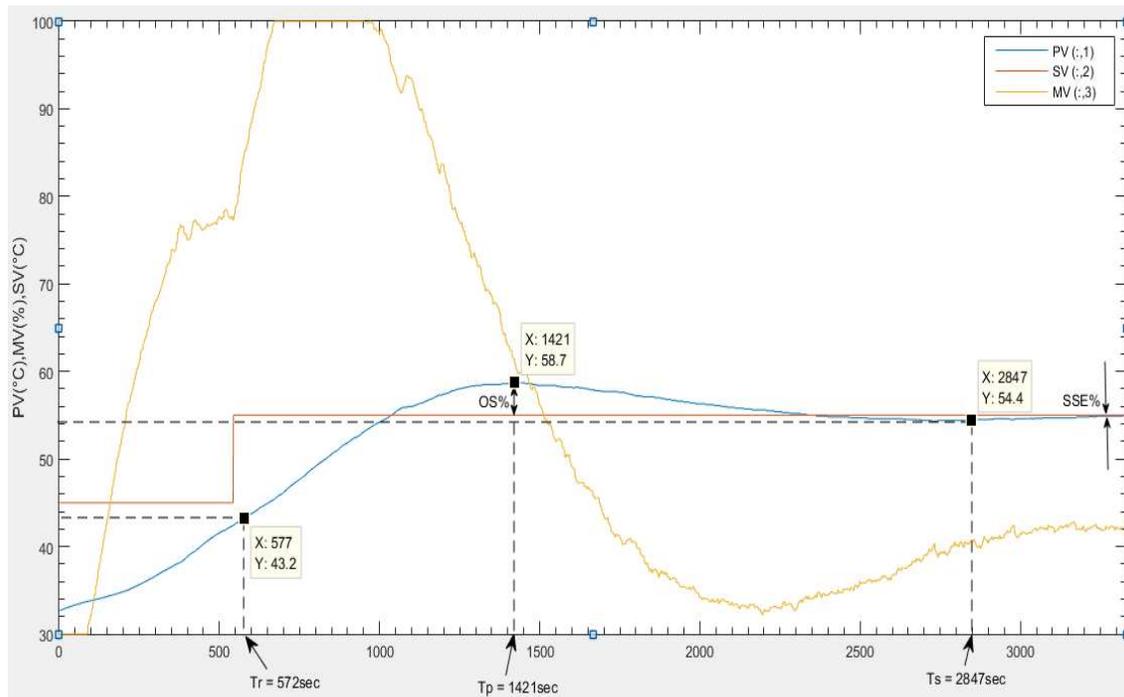


Fig.11. Output response of PID tuning with thermocouple input

Fig. 12, Fig. 13 and Fig. 14 each shows the effect of changing the values of proportional band, T_I and T_D on the temperature being measured with RTD sensor. Differences have been observed in terms of its dynamic response.

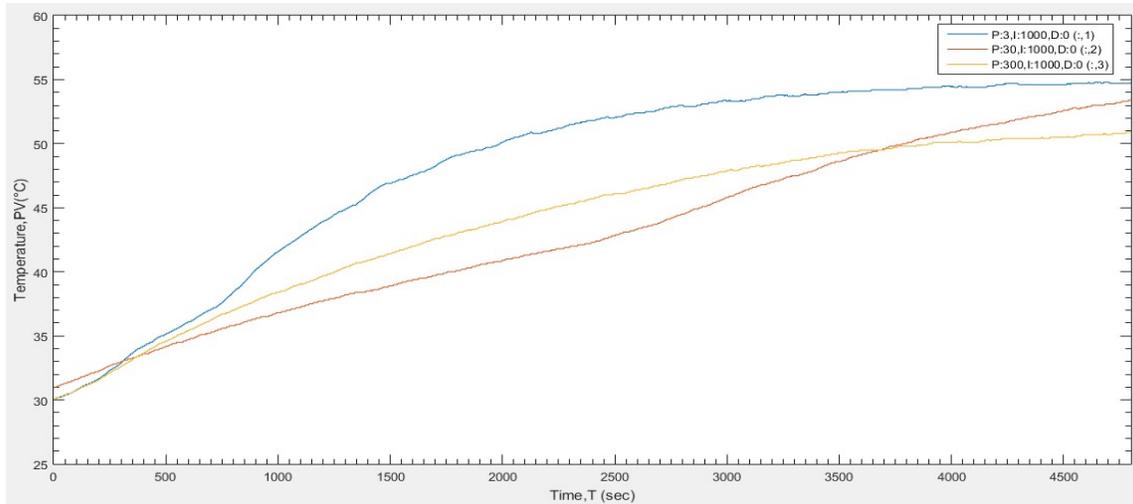


Fig.12. Effect on temperature measured using RTD with change of proportional band

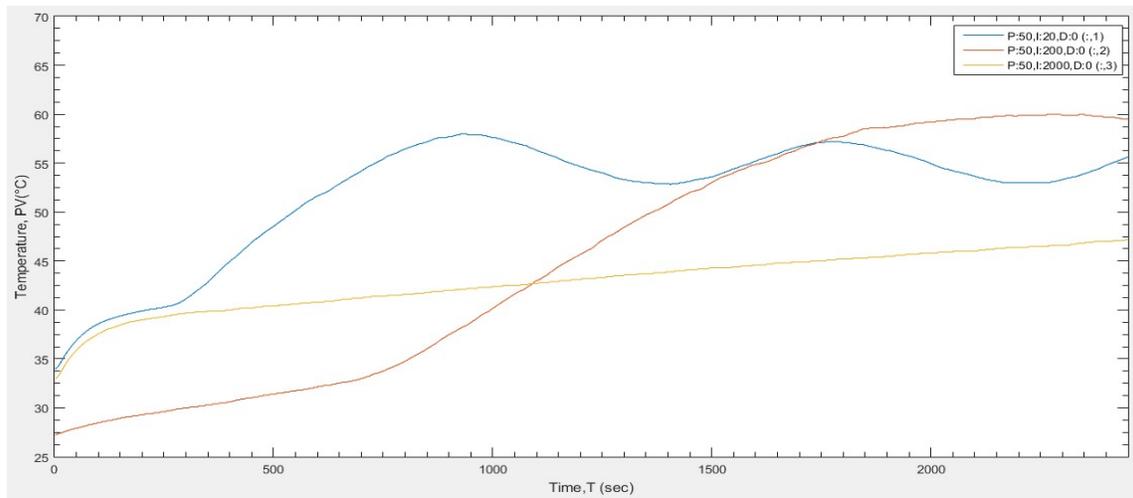


Fig.13. Effect on temperature measured using RTD with change of T_I

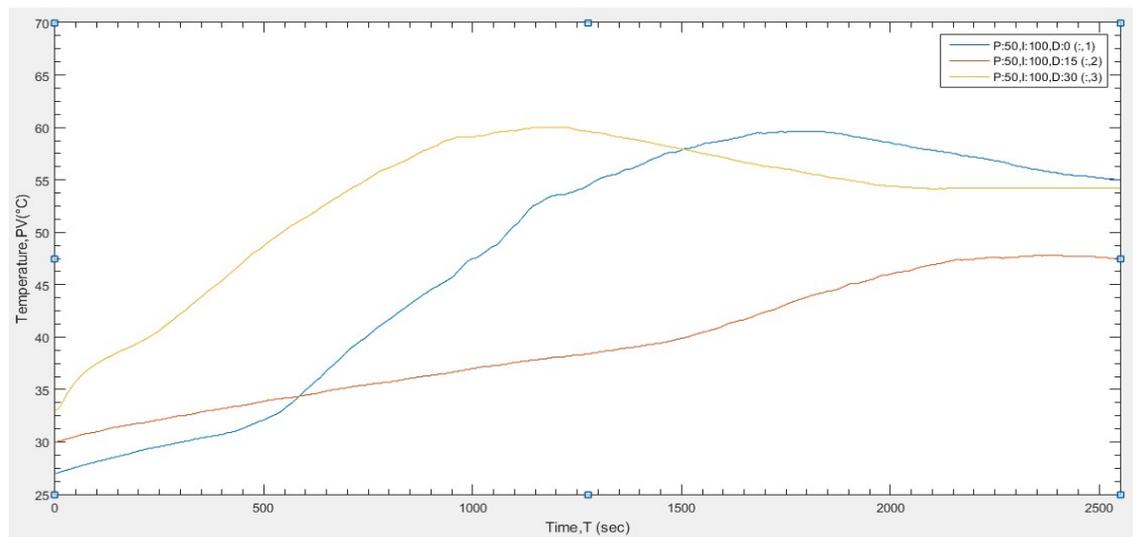


Fig.14. Effect on temperature measured using RTD with change of T_D

Meanwhile, Table 8 summarizes the changes of tuning values that affect temperature measurement through RTD.

Table 8. Effect of tuning values to temperature measurement using RTD

Input	RTD Sensor	Remarks
P	3	Refer to Fig. 12
	30	I = 0 (fixed)
	300	D = 0 (fixed)
		P and D in Offset Mode
I	20	Refer to Fig. 13
	200	P = 50 (fixed)
	2000	D = 0 (fixed)
		D in Offset Mode
D	0	Refer to Fig. 14
	15	P = 50 (fixed)
	30	I = 100 (fixed)

Similarly, Fig. 15, Fig. 16 and Fig. 17 each shows the effect of changing the values of proportional band, T_I and T_D on the temperature being measured using thermocouple sensor. Differences have also been observed in terms of its dynamic response.

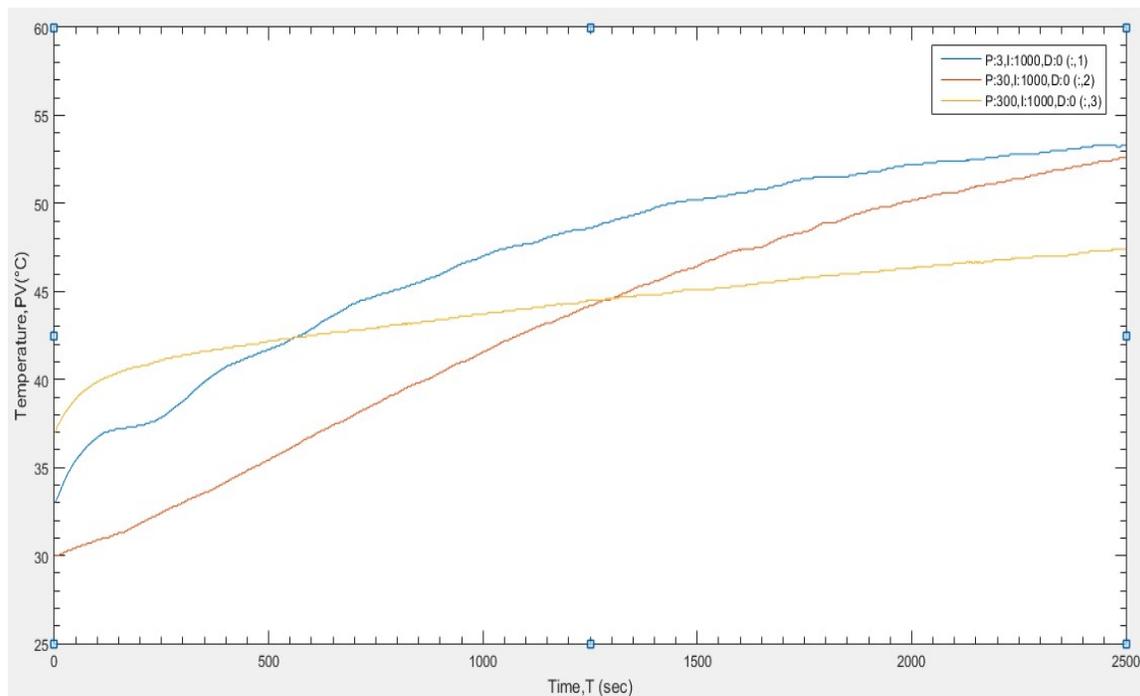


Fig.15.Effect on temperature measured using thermocouple with change of proportional band

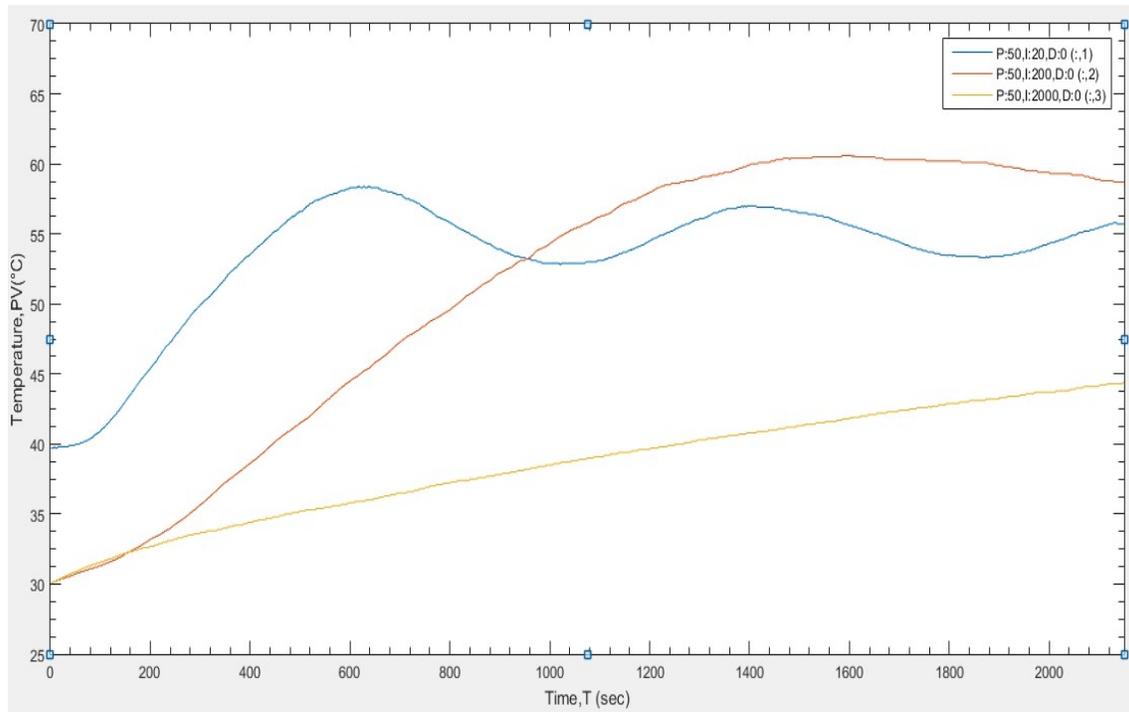


Fig.16.Effect on temperature measured using thermocouple with change of T_I

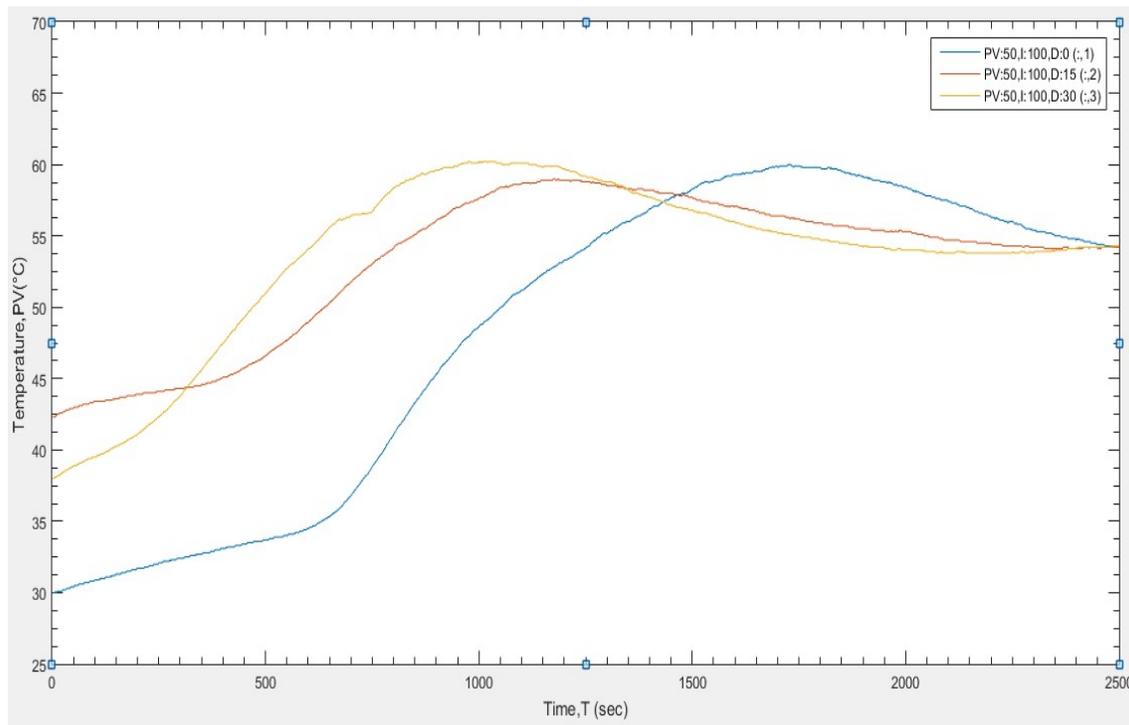


Fig.17.Effect on temperature measured using thermocouple with change of T_D

In addition, Table 9 shows the changes of tuning values that affect temperature measurement through use of thermocouple sensor.

Table 9. Effect of tuning values to temperature measurement using thermocouple sensor

Input		RTD Sensor	Remarks
P	3	Refer to Fig. 15	I = 0 (fixed)
	30		D = 0 (fixed)
	300		P and D in Offset Mode
I	20	Refer to Fig. 16	P = 50 (fixed)
	200		D = 0 (fixed)
	2000		D in Offset Mode
D	0	Refer to Fig. 17	P = 50 (fixed)
	15		I = 100 (fixed)
	30		

7. CONCLUSION

The study has successfully evaluated RTD and thermocouple sensors for PID [19] temperature control [22] in DCS laboratory using Ziegler-Nichols tuning method. Future work will include investigation on other time integral performance criteria such as integral square error, integral absolute error and integral time-weighted absolute error. The task that can be executed in MATLAB Simulink will specifically investigate and improve the error of the process response. Further study can also be done for on and off states, as well as time proportional aspects of process control.

8. ACKNOWLEDGEMENTS

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