# Batch and automated SVI measurements based on short-term temperature variations

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## Abstract

Effects of short-term temperature variations on the sludge volume index (SVI) are evaluated with batch and automated mixed liquor suspended solids (MLSS) settling tests. The test-cylinder environment and meteorological conditions have a direct influence on the MLSS sample temperature ( $T_s$ ). A  $T_s$  change of 4.3°C over the 30 min settling test duration results in an inverse SVI change of 63.0 ml/g, at an average SVI decrease of 14.8 ml/g per 1°C  $T_s$  increase.  $T_s$  compensation or control during routine SVI tests is not common practice, partially due to a lack of temperature-controlled equipment and an absence of  $T_s$ -based MLSS settling models. A practical solution is found to reduce  $T_s$  variations experienced before and during batch MLSS settling tests. An automated MLSS settling meter is used to demonstrate a semi-continuous on-line method to determine SVI at the operational reactor temperature ( $T_r$ ) of a full-scale plant. Basic and best-fit SVI models are obtained from the SVI data generated over diurnal periods, based on MLSS concentration and  $T_r$  fluctuations. These SVI models confirm the inverse dependence of SVI on temperature for the site-specific conditions. A diurnal  $T_r$  fluctuation of 1.8°C results in an SVI change of 26.6 ml/g, at an average -14.8 ml/g SVI change per 1°C  $T_r$  variation.

Keywords: activated sludge, mixed liquor suspended solids (MLSS), model, sludge volume index (SVI), settleability, temperature, wastewater

# Nomenclature

BNR	=	biological nutrient removal
MLSS	=	mixed liquor suspended solids (mg/ $\ell$ )
p value	e =	probability value
$R^2$	=	coefficient of multiple determinations
SVI	=	sludge volume index (mℓ/g)
$SV_{30}$	=	settled sludge volume after 30 min settling in a 1 $\ell$
50		cylinder (mℓ/ℓ)
t-ratio	=	ratio of estimated parameter value to estimated
		parameter standard error
$T_a$	=	ambient temperature (°C)
$T_r$	=	reactor MLSS temperature (°C)
Ť,	=	MLSS sample temperature (°C)
$T_{s30}$	=	MLSS sample temperature after 30 min settling (°C)
$x, x_{p}, x_{s}$	, =	horizontal axis coordinates representing dependable
		variables
у	=	vertical axis coordinate representing response
		variable
α, β, γ	=	regression coefficients
Е	=	random error
$\sigma^2$	=	error variance

#### Introduction

At times biological nutrient removal (BNR) processes suffer from activated sludge or mixed liquor suspended solids (MLSS) settleability problems (Grady and Filipe, 2000) that disturb the

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Received 9 November 2007; accepted in revised form 12 March 2008.

BNR treatment efficiency. Short-term (diurnal) temperature variations in reactor temperature  $(T_p)$  have been observed as having an effect on MLSS settleability (Wilén et al., 2006). Scherfig et al. (1996) showed that  $T_p$  fluctuations are very dependent on local meteorological factors, such as ambient temperature  $(T_a)$ , wind, sunshine and cloud cover. Where MLSS settling properties are traditionally determined batch-wise in 1  $\ell$  size cylinders (Gernaey et al., 1998), it is to be expected that unless special care is taken, these meteorological factors will have an effect on the sample temperature  $(T_s)$ .  $T_s$  is usually not reported in batch MLSS settling evaluations that are used to represent BNR MLSS settleability (Ekama et al., 1997).

Jin et al. (2003) confirm that the traditional sludge volume index (SVI) is still the most widely used index to quantify MLSS settleability for routine operational and design tasks. The SVI has several shortcomings, which prompted Ekama and Marais (1984) and Daigger (1995) to encourage the adoption and use of stirred and diluted indexes. These alternative indexes attempt to standardise the SVI test conditions (Tandoi et al., 2006), but the simplicity of the SVI test procedure ensures its continued general use. Bye and Dold (1998) stated that the main criticism of the SVI is that there is no consistent relationship between SVI and the MLSS concentration, as was experimentally confirmed by Mines and Horn (2004). Dick and Vesilind (1969) noted that this relationship was sensitive to MLSS sample conditions, with container size (width and height), stirring conditions, and temperature considered as key contributors to SVI test result discrepancies. In addition, they cited a study by Rudolphs and Lacy, dated as far back as 1934 (when the SVI test was developed), where  $T_s$ increases were identified as having a considerable and positive influence on MLSS settling and SVI.

The standard methods (*Standard Methods*, 1998) prescribe that  $T_s$  should be kept at  $T_r$  during an SVI test. To ensure that  $T_s$  is stable during an SVI test, and not affected by convection, Simon

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et al. (2005) recommend a maximum 2°C difference between  $T_s$  and  $T_a$  for MLSS settling tests. These reports indicate that the traditional SVI test is temperature dependent, in addition to the well-known MLSS concentration dependence. This temperature dependence of SVI is not linear (Wilén, 1999), therefore empirical SVI correlations are only valid for the relevant experimental  $T_s$  ranges.

There are insufficient guidelines available to describe suitable methods and equipment to control  $T_{e}$ , or to compensate for the differences between  $T_r$  and  $T_s$  during an SVI test. In practice, the SVI test will become more laborious and time-consuming if the MLSS sample must be heated or cooled to T<sub>2</sub> before each test, as well as maintained at  $T_{\mu}$  during the test. Clements (1976) manufactured settling columns fitted with insulation material to stabilise  $T_s$  for SVI tests, while Parker et al. (2000) mentioned that settling columns were used in a temperature-controlled water bath to manage T during MLSS settling tests. Sezgin (1982) reported on the dual use of laboratory-scale reactors as settling vessels to perform SVI tests in situ, which ensured that T was identical to  $T_{r}$ . From the literature survey, no additional details could be found of suitable equipment to manage  $T_{e}$  during SVI tests. Wilén (1999) noted the shortage of temperature-related MLSS settling studies. This survey confirms the lack of information on temperature-controlled MLSS settling equipment and methods.

The authors evaluated an on-line semi-continuous SVI determination method that incorporates temperature variations. A custom-designed automated MLSS settling meter was commissioned at a BNR reactor outlet to provide MLSS settling profiles and SVI data at the operational T. Vanrolleghem et al. (2006) regard the use of on-line MLSS settling meters as a suitable technique to generate MLSS settling profiles at full-scale plant reactors. Technological progress makes the future development of reliable MLSS settling meters more commonplace (Gernaey et al., 1998), after Sekine et al. (1989) commissioned an automated MLSS settling and SVI meter about 20 years ago to perform batch settling tests. Vanderhasselt et al. (1999) developed an on-line MLSS settling meter to provide semi-continuous settling profiles for settling velocity studies. These on-line MLSS settling profiles and associated SVI values will follow the diurnal MLSS concentration fluctuation in the reactor.

This MLSS concentration fluctuation is created due to the diurnal reactor inflow and return activated sludge solids concentration fluctuations (Härtel and Pöpel, 1992). The  $T_r$  follows in similar fashion a diurnal sinusoidal profile related to the  $T_a$  profile, as modelled by Makinia et al. (2005). Hence, on-line SVI determinations will ensure that the SVI profile reflects operational reactor conditions, not only in terms of MLSS concentration, but also with regard to  $T_r$ .

The purpose of this paper is to demonstrate that an automated MLSS settling meter can effortlessly incorporate temperature in SVI tests. This paper comprises three main components. Firstly, the extent of  $T_s$  variations during batch SVI tests is examined in terms of the MLSS sample environment. Secondly, an MLSS settling meter is used to obtain SVI profiles, according to diurnal MLSS concentration and  $T_r$  fluctuations in a full-scale reactor. Finally, a basic model is developed that represents an improved temperature-based SVI correlation.

## Experimental

Grab MLSS samples were sourced during winter from the outlet of a full-scale BNR reactor. Batch MLSS settling tests commenced on plant location within minutes of sampling. This ensured that fresh MLSS samples were used with minimal changes in  $T_s$ . Two 1  $\ell$  and two 2  $\ell$  graduated polypropylene cylinders (61.0 and 77.0 mm diameter, 342.5 and 429.5 mm height respectively) were filled with MLSS samples and placed next to each other to create similar environmental conditions ( $T_a$  and solar radiation). To change these environmental conditions, the cylinders were moved into direct sunlight or shade. The settled MLSS volume was noted periodically, starting at every minute up to 10 min, then every second minute up to 20 min, and finally every 5 min up to 30 min. These 17 data points created a 30 min MLSS settling profile. To obtain a 30 min settled volume (SV<sub>30</sub>) based on a 1  $\ell$  MLSS sample, the final settled volume in the 2  $\ell$  cylinder was divided by 2. The SVI was calculated by dividing this SV<sub>30</sub> (m $\ell/\ell$ ) by the initial MLSS concentration (g per  $\ell$ ) (*Standard Methods*, 1998) from each settling profile.

An on-line and a hand-held MLSS concentration meter (Royce models 9100D and 711) supplied the reactor and sample MLSS concentrations. The built-in temperature sensor of an online dissolved oxygen concentration meter (Royce 7011A) and an electronic data logger (Fourier, MicroLogPlus) measured and recorded the  $T_r$  data. This logger had a limited 0.3°C increment storage facility. The T<sub>e</sub> was measured with a hand-held digital thermometer (Testo 925). This meter was fitted with a 0.6 m long immersion probe that could reach the centre of the MLSS sample inside the test cylinder. The  $T_a$  was measured during batch SVI tests in sunshine and in shade with a hand-held dissolved oxygen concentration meter (YSI, Model 550A), equipped with a built-in thermometer. The on-line  $T_a$  was recorded with a second logger equipped with an internal temperature sensor. The on-line MLSS concentration data were recorded every 5 min with a third logger (MC Systems, Alog MCS131LCD). MLSS concentration meter sensors were cleaned daily and calibrated on a regular basis.

An automated MLSS settling meter (2  $\ell$  perspex cylinder, 84.0 mm diameter, and 360.9 mm height) was commissioned at a full-scale BNR reactor. The settling meter generated 85 MLSS settling profiles and associated SVI readings over 2 d. The SVI data points were combined with the initial MLSS concentration and average  $T_r$  over 30 min settling periods, and fitted with Microsoft Excel, as well as a statistical software package (DataFit, 2005). DataFit contains 242 predefined non-linear regression models, up to 10-parameter polynomial functions. Polynomial functions trend data points with sinusoidal wave profiles, as found in diurnal  $T_a$  (Scherfig et al., 1996) and  $T_r$  (Makinia et al., 2005) fluctuations. From the shape of the profile, the amplitude (height of wave) and wavelength (distance between wave crests) illustrate the diurnal fluctuations.

The statistical significance of a model, to account for the fraction of the variation among the data points represented by the model, is illustrated by the coefficient of multiple determinations ( $\mathbb{R}^2$ ). Researchers have used  $\mathbb{R}^2$  as a general indicator of the statistical significance of settleability models (Daigger, 1995; Ekama et al., 1997), based on batch SVI data sets. The following 3-parameter 1<sup>st</sup> order polynomial function was chosen as the fitted regression model for SVI, based on  $\mathbb{R}^2$  and formula simplicity:

$$y = \alpha + \frac{\beta}{x_1} + \frac{\gamma}{x_2} + \varepsilon, \quad \varepsilon \approx n(0, \sigma^2)$$

where: y is the SVI (m $\ell$ /g)

 $x_1$  is the MLSS concentration (mg/ $\ell$ )  $x_2$  is the T<sub>r</sub> (°C)  $\alpha$ ,  $\beta$ ,  $\gamma$  are regression constants

 $\varepsilon$  is the random error

 $\sigma^2$  is the error variance

TABLE 1   Effect of batch MLSS settling cylinder environment on T <sub>ree</sub> and SVI							
Cylinder	Placement	Parameter	Sample 1	Sample 2	Sample 3	Average	SVI change
size (ℓ)		MLSS	4 210	3 930	4 470	4 203	
		concentration (mg/l)					
		$T_r(^{\circ}\mathrm{C})$	18.0	19.7	21.0	19.6	
		$T_a$ (°C)	16.9	17.5	19.4	17.9	
1	Shade	SVI (mℓ/g)	181	170	172	174	- 66 mℓ/g·4.4°C
		$T_{s30}$ (°C)	17.0	19.5	20.9	19.1	or
1	Sunshine	SVI (mℓ/g)	105	104	116	108	-15.0 mℓ/g·1°C
		$T_{s30}$ (°C)	21.5	23.8	25.2	23.5	
2	Shade	SVI (mℓ/g)	195	137	181	171	- 60 mℓ/g·4.1°C
		$T_{s30}$ (°C)	17.0	19.5	20.7	19.1	or
2	Sunshine	SVI (mℓ/g)	109	106	119	111	] -14.6 mℓ/g·1°C
		$T_{_{\rm s30}}(^{\circ}{\rm C})$	20.9	23.6	25.1	23.2	

## **Results and discussion**

#### Batch SVI dependence on environment and T<sub>s</sub>

Three sets of manual batch MLSS settling tests, at an average sample MLSS concentration of 4 203 mg/ $\ell$ , were completed at an average  $T_r$  and  $T_a$  of 19.6 and 17.9°C respectively. Table 1 indicates that a  $T_s$  increase of 4.3°C, due to cylinder placement in sunshine during the 30 min test, caused an average SVI decrease of 63 m $\ell$ /g. The  $T_s$  of the 1  $\ell$  and 2  $\ell$  cylinders increased, from 19.1°C at the start of the settling test, to 23.5 and 23.2°C respectively after 30 min ( $T_{s30}$ ). The corresponding SVI in the 1  $\ell$  and 2  $\ell$  cylinders decreased from 174 and 171 m $\ell$ /g to 108 and 111 m $\ell$ /g respectively.

The cylinder size played a minor role in SVI variations, as the larger 2  $\ell$  cylinder heated up more slowly to 23.2°C, against a  $T_{s30}$  of 23.5°C for the smaller 1  $\ell$  cylinder. The  $T_s$  difference, due to cylinder size, was reflected in the slightly higher SVI of 111 m $\ell$ /g in the colder 2  $\ell$  cylinder, against 108 m $\ell$ /g in the warmer 1  $\ell$  cylinder. The SVI change in the 1  $\ell$  and 2  $\ell$  cylinders was an average 15.0 m $\ell$ /g and 14.6 m $\ell$ /g SVI decrease respectively per 1°C T<sub>s</sub> increase, leading to an average 14.8 m $\ell$ /g SVI decrease per 1°C T<sub>s</sub> increase.

Solar radiation is the main energy source for heat gain in quiescent water bodies (Gillot and Vanrolleghem, 2003). Atmospheric radiation, surface convection, and wall convection/conduction are additional energy contributors in an MLSS sample heat balance (Makinia et al., 2005). The effects of these energy sources on  $T_s$  and SVI over the 30 min test period were clearly demonstrated in the experimental results in Table 1.

These observations illustrate the importance of recording proper reference conditions during MLSS settling and SVI tests. In this study, experimental conditions were limited to a narrow  $T_r$  and  $T_s$  range on a short-term basis to simulate conditions at an operational plant. The  $T_s$  adjusts towards the  $T_a$  of the immediate environment in which the tests are performed, such as outdoors at the  $T_a$  of a plant reactor, or indoors at the  $T_a$  in a laboratory. The  $T_s$  could vary considerably from the  $T_r$  (colder or warmer), depending on  $T_a$ , the sample environment, as well as the time delay between MLSS sampling and sample testing.

Dick and Vesilind (1969) concluded that an SVI reading was only meaningful when supplied with the MLSS concentration, as the MLSS concentration exerted the largest influence on the SVI. Bye and Dold (1998) proposed that the dimensions of the settling vessel be included in MLSS settling test results. These improved settleability reporting methods could be further enhanced by recording information about temperature  $(T_r, T_s)$ , and  $T_a$  and environmental conditions during MLSS settling and SVI tests.

#### On-line SVI dependence on MLSS concentration and T,

The direct relationship between MLSS concentration and SVI is illustrated in Fig. 1 (next page) for a 48 h period, based on online data. The MLSS concentration fluctuation follows a sinusoidal wave profile, in accordance with profiles observed by Härtel and Pöpel (1992). This cyclic MLSS concentration fluctuation of between 4 489 and 4 923 mg/ $\ell$  is mirrored without significant lag by the SVI fluctuation of between 97 and 203 m $\ell$ /g. MLSS concentration and SVI fluctuate in a matching diurnal relationship with fluctuations of 434 mg/ $\ell$  and 106 m $\ell$ /g respectively.

The mathematical relationships between settleability parameters are approximated as basic polynomial functions, to show trends that adequately describe MLSS settleability behaviour. The MLSS concentration data points over the 2 d period are thus represented by a polynomial function, as shown in Fig. 1, with an amplitude of about 217 mg/ $\ell$  and  $R^2 = 0.90$ . The separate slope change over the first 6 h of the MLSS concentration profile, representing a change of about 200 mg/ $\ell$ , can be attributed to experimental conditions. The SVI data points are described by a similar polynomial function, with an amplitude of about 53 m $\ell$ /g and  $R^2 = 0.91$ .

The MLSS concentration and SVI relationship can be represented in Fig. 2 by a linear and a polynomial function, with comparable  $R^2$  values of 0.67 and 0.68 respectively. Large scatter of SVI data points around average values is evident for both trends. The data scatter is in agreement with earlier observations of experimental MLSS settling data and calculated SVI data ranges, as presented in models by Daigger and Roper (1985) and Catunda and Van Haandel (1992). There are therefore other significant factors present that are not incorporated in the traditional SVI regression models based only on MLSS concentration. Ambient and reactor temperature fluctuations, and the related change in sample temperature, are such factors which can account for some of the scatter in SVI data.

The relationship between  $T_a$  and  $T_r$  at the assessed reactor is shown in Fig. 3 over a 48 h period.  $T_r$  follows the cyclic wave shape of  $T_a$ , with a lag of about 8 h. The characteristic sinusoidal profile of the  $T_a$  data consists of successive warming and cooling stages during day- and night-time, as modelled by Makinia et al. (2005). The  $T_r$  response to  $T_a$  fluctuations can be adequately presented by polynomial trends.





Figure 4 Experimental data and fitted curves of temporal variations in SVI and T,

 $T_a$  fluctuates between 14.0 and 31.7°C, and  $T_r$  follows with a fluctuation of between 17.2 and 19.0°C. The  $T_a$  data points over 2 d are represented by a polynomial function with an amplitude of about 8.9°C and  $R^2 = 0.80$ . The response from  $T_r$  is described by a similar polynomial function with an amplitude of about 0.9°C and  $R^2 = 0.90$ .

The on-line SVI and  $T_r$  profiles, as shown in Figs. 1 and 3 respectively, are combined in Fig. 4. The cyclic fluctuation of SVI inversely follows the  $T_r$  fluctuation profile, without significant lag. The extended horizontal portions of the  $T_r$  profile are formed by the limited 0.3°C recording increments of the data logger.

It has been demonstrated that the SVI follows direct and inverse relationships with the MLSS concentration and  $T_r$ respectively, confirming the results of earlier studies (Dick and Vesilind, 1969). The periodic cyclic fluctuations of SVI, MLSS concentration and  $T_r$  are related to the diurnal  $T_a$  cycle.

The experimental MLSS concentration and  $T_r$  data obtained from the MLSS settling meter, as illustrated in Figs. 1 and 4, are summarised in Table 2. These data represent the modelled SVI range, as well as the corresponding MLSS concentration and  $T_r$ limits of this SVI model.

The following simplified regression model, with  $R^2 = 0.71$ , provides the SVI response relationship with MLSS concentration and  $T_r$  variations:

$$SVI = 872.4 - \frac{4624176.1}{MLSS} + \frac{4823.4}{T_r} \text{ (ml/g)}$$
(1)

The regression variable results are summarised in Table 3, including the standard error and the 95% confidence intervals. The large *t*-ratios confirm that all parameters are significant, with MLSS concentration having the largest influence in the model. The low *p* values indicate that none of the parameters can be removed from the model without affecting the regression model accuracy, with a smaller than 1% chance that  $T_r$  is zero. A calculated correlation coefficient of 0.512 between the estimates of  $\beta$  and  $\gamma$  shows that the effect of MLSS concentration or  $T_r$  on SVI can not be independently determined with the present data set to provide similar model accuracies.

The plot of this model, valid only within the experimental data ranges listed in Table 2, is presented in Fig. 5. The threedimensional graph illustrates the model, where the colour-coded surface areas represents the regression results, colour bands represent SVI changes of about 15 ml/g, and the bullets represent the experimental data points. The  $x_1$ -axis represents the MLSS concentration range of 4 489 to 4 923 mg/l, the  $x_2$ -axis represents the  $T_r$  range from 17.2 to 19.0°C, and the *y*-axis represents the modelled SVI from 96 to 214 ml/g. The modelled SVI range slightly exceeds the experimental SVI range of 97 to 203 ml/g.

TABLE 2   Modelled SVI range, with experimental MLSS concentration and T, limits						
Parameter	Unit	Lowest SVI, minimum MLSS concentration, Maximum t <sub>r</sub>	Intermediate SVI, Minimum MLSS concentration, Minimum t <sub>r</sub>	Intermediate SVI, Maximum MLSS concentration, Maximum t,	Highest SVI, Maximum MLSS concentration, Minimum t <sub>r</sub>	
SVI	(mℓ/g)	96	118	187	214	
MLSS concentration	(mg/ℓ)	4489	4489	4923	4923	
T <sub>r</sub>	(°C)	19.0	17.2	19.0	17.2	

TABLE 3							
Regression variable results							
Variable	Value	Standard error	Lower limit	Upper limit	t-ratio	p value	
α	872.4	159.1	555.9	1188.9	5.48	0.0000	
β	-46241761	445895.9	-5511196.8	-3737155.4	-10.4	0.0000	
γ	4823.4	1611.6	1617.5	8029.3	2.99	0.0037	



Figure 5 Experimental data points and modelled three-dimensional response surface of SVI (y) over the dependable variables MLSS concentration (x,) and T<sub>r</sub>(x<sub>2</sub>)

The SVI dependence on the full-scale  $T_r$  can be illustrated with a simulation. The SVI decrease, due to a  $T_r$  increase from 17.2 to 19.0°C, is calculated with the simplified SVI-model (Eq. (1)). The SVI decreases at a constant MLSS concentration of 4 500 mg/ $\ell$  by 26.5 m $\ell/g$ , from 125 to 98.5 m $\ell/g$ , for the corresponding 1.8°C  $T_r$  increase. Under these conditions, the inverse SVI relationship with  $T_r$  is averaged at -14.8 m $\ell/g$  SVI per 1°C  $T_r$  variation. This relationship is also correlated by a best-fit 10 parameter 10<sup>th</sup> order polynomial function, with  $R^2 = 0.84$ .

The SVI relationship with  $T_r$  was not investigated over an extended temperature range outside the operational  $T_r$  and  $T_s$  variations. Several previous studies (Cetin and Sürücü, 1990; Krishna and Van Loosdrecht, 1999; Morgan-Sagastume and Allen, 2003; Zhang et al., 2006) reported poorer MLSS settling at elevated temperatures. SVI values increased (up to 540 ml/g) at long-term elevated temperatures as high as 35 to 45°C. These extreme temperature conditions usually result in the interruption of floc formation (Gerardi, 2002) and deflocculation. Wilén (1999) experimentally confirmed deflocculation and the resulting reduced MLSS settling properties at high  $T_s$  of 30 to 45°C, as well as at low  $T_s$  of 4°C. Some of the reported MLSS settling deteriorations at elevated temperatures could be attributed to industrial wastewater plant conditions or to long-term high temperature-based conditions, as well as to MLSS concentration variations.

Wilén (1999) confirms that activated sludge responds differently to different temperatures. The conflicting effects of temperature on SVI illustrate the importance of proper reference conditions during MLSS settling evaluations and SVI tests. In this study, experimental conditions were limited to the typical  $T_r$  and  $T_s$  variations on a short-term basis, mainly to exclude the influence of micro-organism population changes on MLSS settleability. These arrangements reproduced operational plant and laboratory conditions where MLSS settling and SVI improved at increased temperatures.

Dick and Vesilind (1969) cautioned against operational and research decisions that rely on batch SVI test results as the primary measurement of MLSS characteristics. The MLSS sample environment in small cylinders can create artificial experimental settling conditions (Sezgin, 1982). The sensitivity of the calculated SVI to environmental conditions of the MLSS sample, and specifically temperature, has been illustrated. The use of batch SVI test results, without considering these experimental conditions, may lead to over- or under-design, or the implementation of inappropriate process control measures at wastewater treatment plants.

#### Summary

In this paper, it is demonstrated that short-term temperature variations are an essential component of batch MLSS settling and SVI tests. The experimental results show that the SVI is highly dependent on MLSS sample conditions and experimental procedures. An inverse SVI variation of about 14.8 ml/g per 1°C temperature change has been established during batch and on-line MLSS settling tests, valid for the specific experimental conditions of this study. Solar radiation changes and diurnal  $T_r$  fluctuations created the variable temperature conditions investigated during the batch and automated on-line SVI tests respectively.

The SVI correlation with MLSS concentration at  $R^2 = 0.67$ improves to  $R^2 = 0.71$  when  $T_r$  is included in a simplified first order settling model. This model can be further improved to  $R^2$ = 0.84 with a best-fit 10<sup>th</sup> order model. The traditional experimental procedures to establish these temperature-based batch MLSS settling correlations and related SVI data are laborious and time- consuming. Automated MLSS settling meters provide semi-continuous settling profiles and SVI data that reflect the operational diurnal  $T_r$  profile. The SVI data sets generated by such an MLSS settling meter are suitable for the development of empirical settling models for individual plant reactors.

# Conclusions

The main conclusions drawn from this research are as follows:

- The rise in sample and reactor temperatures, during batch and on-line MLSS settling tests respectively, caused considerable SVI reductions. The average SVI decrease of 14.8 ml/g per 1°C increase is based on both batch and on-line SVI measurements. These SVI correlations are valid only for the experimental MLSS sample conditions, with regard to MLSS concentration, temperature, and experimental procedure. The SVI correlations should not be extrapolated outside experimental conditions, but rather redeveloped for site-specific operational conditions.
- A small, but statistically significant improvement is obtained when  $T_r$  is included in MLSS settling correlations. A multiple correlation between SVI and 1/MLSS concentration improves from  $R^2 = 0.67$  to 0.71 when it is expanded to include  $1/T_r$ . A best-fit model between SVI, MLSS concentration, and  $T_r$ , confirms the improved correlation and benefit of  $T_r$  inclusion in SVI measurements, with  $R^2$  increasing from 0.67 to 0.84.
- An automated MLSS settling meter is a valuable tool that calculates the temperature dependant SVI values automatically from the semi-continuous settling profiles. Time-consuming experimental work is avoided to manage  $T_s$  at the operational  $T_r$  during MLSS settling tests.

With the above conclusions, a suitable approach is provided to improve the reliability of SVI, as the effects of short-term temperature variations can be practically eliminated from SVI tests.

## Acknowledgements

The Water Research Commission financially supported this research, and ERWAT provided facilities and research resources. Mr G George is acknowledged for his contribution during the construction and commissioning of the MLSS settling meter. The authors express their appreciation to Prof FE Steffens and Dr MJ van der Linde of the Department of Statistics, University of Pretoria, for their comments on the statistical interpretation of the experimental data.

# References

- BYE CM and DOLD PL (1998) Sludge volume index settleability measures: effect of solids characteristics and test parameters. *Water Environ. Res.* **70** (1) 87-93.
- CATUNDA PFC and VAN HAANDEL AC (1992) Activated sludge settling. Part I: Experimental determination of activated sludge settleability. *Water SA* **18** (3) 165-172.
- ÇETIN FD and SÜRÜCÜ G (1990) Effects of temperature and pH on the settleability of activated sludge flocs. *Water Sci. Technol.* 22 (9) 249-254.
- CLEMENTS MS (1976) The application of static column tests to sedimentation tank design. *Water Pollut. Control* **75** (3) 360-376.
- DAIGGER GT and ROPER RE (Jr.) (1985) The relationship between SVI and activated sludge settling characteristics. J. Water Pollut. Control Fed. 57 (8) 859-866.
- DAIGGER GT (1995) Development of refined clarifier operating diagrams using an updated settling characteristics database. *Water Environ. Res.* 67 (1) 95-100.
- DATAFIT (2005) Oakdale Engineering, Statistical Software Package, Version 8.1.69, Evaluation Copy, US. <u>http://www.curvefitting.com</u> (Accessed on 15/01/2005).
- DICK RI and VESILIND PA (1969) The Sludge Volume Index What is it? J. Water Pollut. Control Fed. 41 (7) 1285-1291.
- EKAMA GA and MARAIS GVR (1984) Two improved activated sludge settleability parameters. *IMESA* 6 (9) 20-26.
- EKAMA GA, BARNARD JL, GÜNTHERT FW, KREBS P, McCORQUODALE JA, PARKER DS and WAHLBERG EJ (1997) Secondary Settling Tanks: Theory, Modelling, Design and Operation. IAWQ Scientific and Technical Report No. 6. IWA Publishing, Simpson Drewett and Co. Ltd., Richmond, Surrey, England.
- GERARDI MH (2002) Settleability Problems and Loss of Solids in the Activated Sludge Process. John Wiley & Sons, Hoboken, New Jersey, USA.
- GERNAEY K, VANDERHASSELT A, BOGAERT H, VANROL-LEGHEM P and VERSTRAETE W (1998) Sensors to monitor biological nitrogen removal and activated sludge settling. J. Microbiol. Methods **32** 193-204.
- GILLOT S and VANROLLEGHEM PA (2003) Equilibrium temperature in aerated basins-comparison of two prediction models. *Water Res.* **37** 3742-3748.
- GRADY CPL (Jr.) and FILIPE CDM (2000) Ecological engineering of bioreactors for wastewater treatment. *Water Air Soil Pollut.* **123** 117-132.

- HÄRTEL L and PÖPEL HJ (1992) A dynamic secondary clarifier model including processes of sludge thickening. *Water Sci. Technol.* **25** (6) 267-284.
- JIN B, WILÉN BM and LANT P (2003) A comprehensive insight into floc characteristics and their impact on compressibility and settleability of activated sludge. *Chem. Eng. J.* 95 (1-3) 221-234.
- KRISHNA C and VAN LOOSDRECHT MCM (1999) Effect of temperature on storage polymers and settleability of activated sludge. *Water Res.* 33 (10) 2374-2382.
- MAKINIA J, WELLS SA and ZIMA P (2005) Temperature modeling in activated sludge systems: A case study. *Water Environ. Res.* 77 (5) 197-204.
- MINES RO and HORN CR (2004) Misconceptions about unstirred SVI. Proc. 2004 World Water and Environmental Resources Congress. 27 June – 1 July, Salt Lake City, USA.
- MORGAN-SAGASTUME F and ALLEN DG (2003) Effects of temperature transient conditions on aerobic biological treatment of wastewater. *Water Res.* **37** (15) 3590-3601.
- PARKER DS, WAHLBERG EJ and GERGES HZ (2000) Improving secondary clarifier performance and capacity using a structured diagnostic approach. *Water Sci. Technol.* **41** (9) 201-208.
- SCHERFIG J, SCHLEISNER L, BRØND S and KILDE N (1996) Dynamic temperature changes in wastewater treatment plants. *Water Environ. Res.* 68 (2) 143-151.
- SEKINE T, TSUGURA H, URUSHIBARA S, FURUYA N, FUJIMOTO E and MATSUI S (1989) Evaluation of settleability of activated sludge using a sludge settling analyser. *Water Res.* 23 (3) 361-367.
- SEZGIN M (1982) Variation of sludge volume index with activated sludge characteristics. *Water Res.* 16 83-88.
- SIMON J, WIESE J and STEINMETZ H (2005) Results of field tests and possible applications for *in-situ* sludge volume probes. Proc. 2<sup>nd</sup> IWA-ICA Conference. 29 May – 2 June, Busan, South Korea.
- STANDARD METHODS (1998) Standard Methods for the Examination of Water and Wastewater (20<sup>th</sup> edn.) American Public Health Association (APHA)/American Water Works Association (AWWA)/ Water Environment Federation (WEF), Washington, D.C., USA.
- TANDOI V, JENKINS D and WANNER J (2006) Activated Sludge Separation Problems: Theory, Control Measures, Practical Experience. IWA Scientific and Technical Report No. 16, IWA Publishing, London, England.
- VANDERHASSELT A, ASPEGREN H, VANROLLEGHEM P and VERSTRAETE W (1999) Settling characterisation using on-line sensors at a full-scale wastewater treatment plant. *Water SA* **25** (4) 453-458.
- VANROLLEGHEM PA, CLERCQ BD, CLERCQ JD, DEVISSCHER M, KINNEAR DJ and NOPENS I (2006) New measurement techniques for secondary settlers: A review. *Water Sci. Technol.* 53 (4-5) 419-429.
- WILÉN BM (1999) Properties of Activated Sludge Flocs. Paper VI. Effect of Temperature and Cold-Storage on Activated Sludge Floc Strength. Ph.D. Thesis, Dissertation No 15, Department of Sanitary Engineering, Chalmers University of Technology, Göteborg, Sweden.
- WILÉN BM, ONUKI M, HERMANSSON M, LUMLEY D and MINO T (2006) Influence of flocculation and settling properties of activated sludge in relation to secondary settler performance. *Water Sci. Technol.* 54 (1) 147-155.
- ZHANG S, YANG F, LIU Y, ZHANG X, YAMADA Y and FURU-KAWA K (2006) Performance of a metallic membrane bioreactor treating simulated distillery wastewater at temperatures of 30 to 45°C. Desalination 194 146-155.